



**UTM**  
UNIVERSITI TEKNOLOGI MALAYSIA



**AMTEC**  
Advanced Membrane Technology  
Research Centre

# Opportunities in Membrane Technology in Water Resources

Advanced Membrane Technology Research Centre (AMTEC)  
Universiti Teknologi Malaysia (UTM), Malaysia

# Presentation Outline

1. Introduction
2. Membrane Applications
3. Nanomaterials in Membrane Technology
4. Advanced Membrane Technology
  - i. Forward Osmosis
  - ii. Photocatalytic membrane
5. Concluding Remarks







# Global Water Crisis:

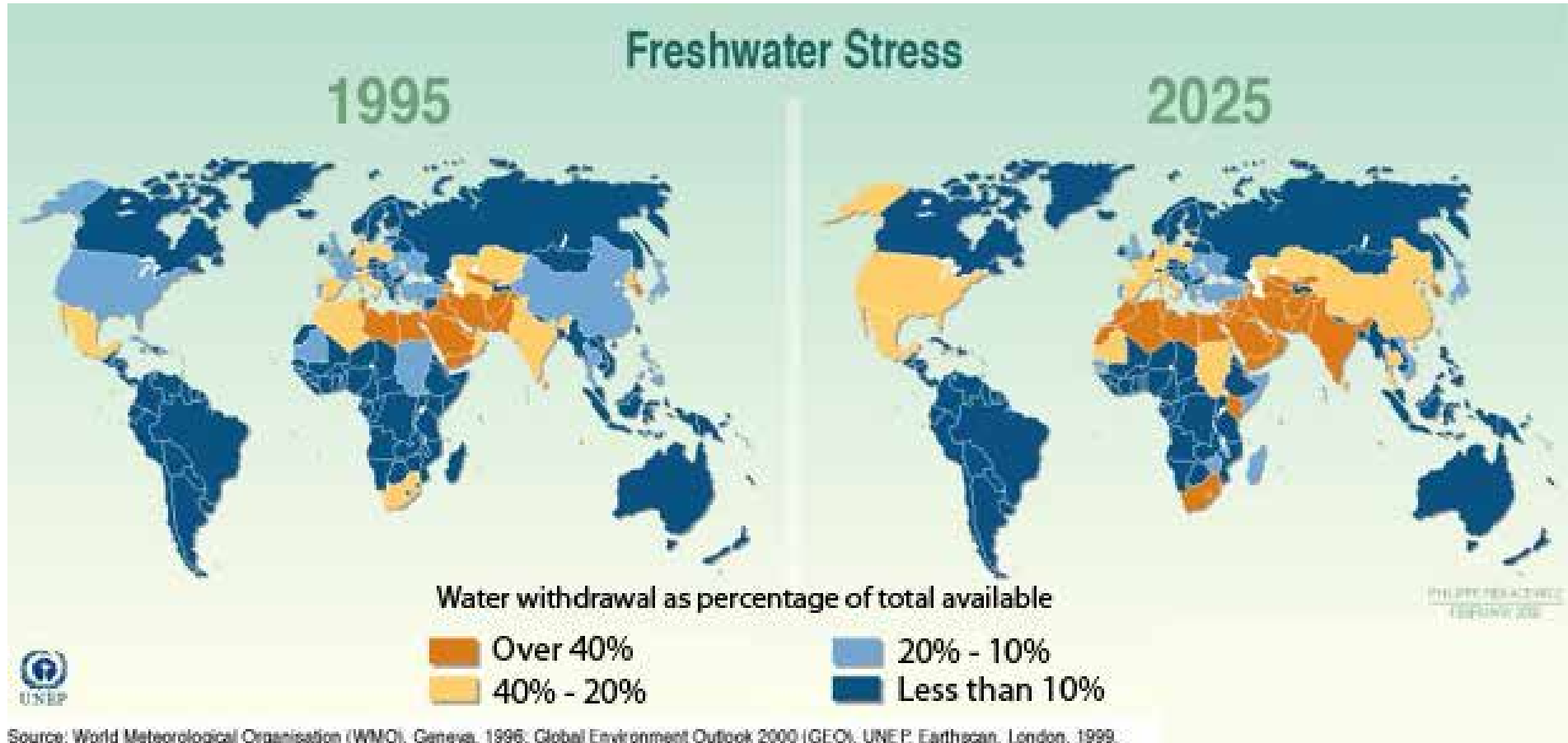
## H<sub>2</sub>O QUICK FACTS

# Do you know that...

- Over the past 40 years the world's population has doubled and use of water has quadrupled.
- 783 million people (1 in 10 people) do not have access to clean and safe water.
- In developing countries, as much as 80% of illnesses are linked to poor water and sanitation conditions.
- Compared to today, five times as much land is likely to be under "extreme drought" by 2050.
- By 2050, 1 in 5 developing countries will face water shortages.

*Sources: United Nation's Food and Agriculture Organization; World Health Organization; UNICEF, 2015*

# Water-stress Regions-A Worsening Scenario



*Sources: World Meteorology Organization*

# Factors Leading to Water Crisis



Climate and Geography



Poor Water Infrastructure  
and Sanitary



Water Pollutions

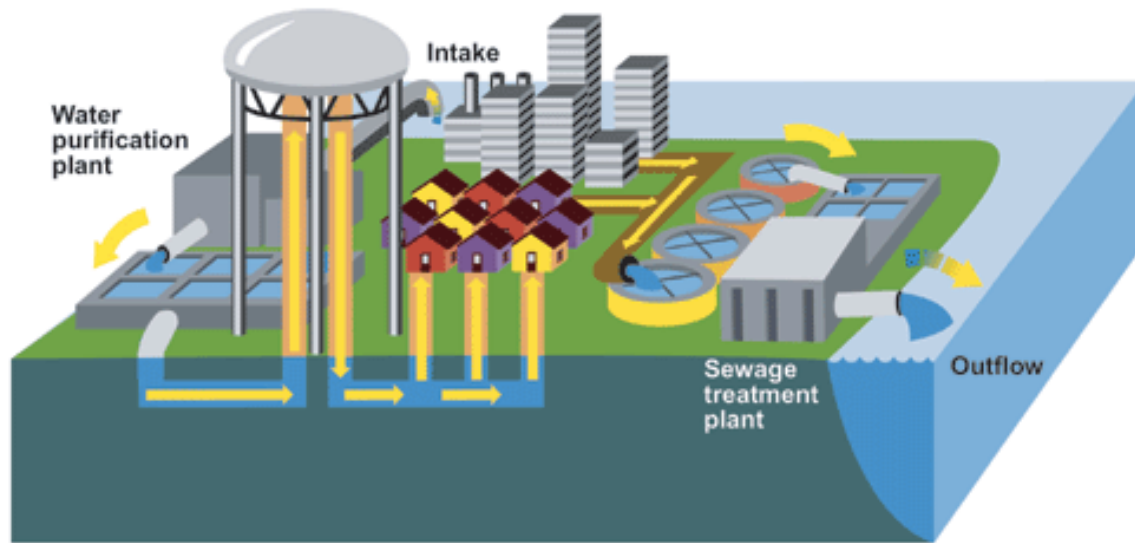


# Can Membrane Cope?

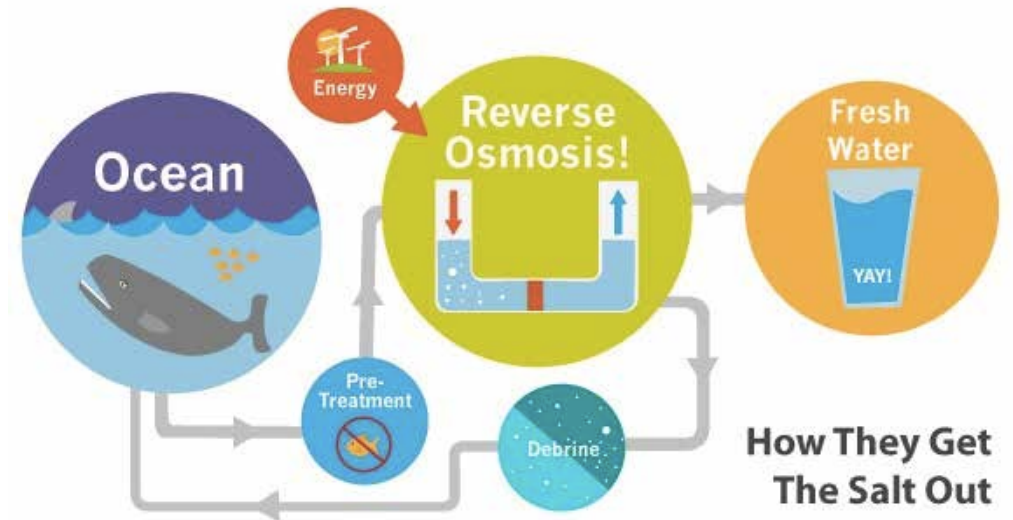


# Engineering Solutions: Membrane Technology

## Wastewater Treatment



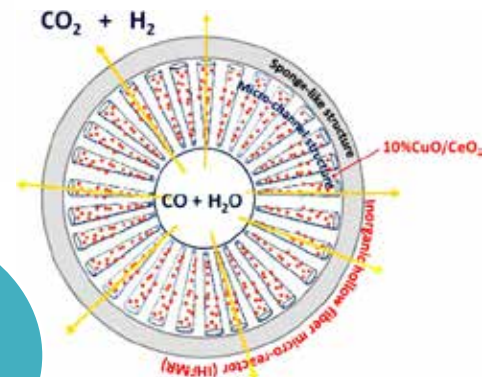
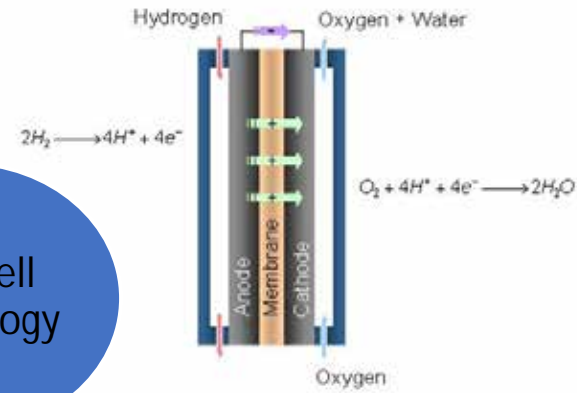
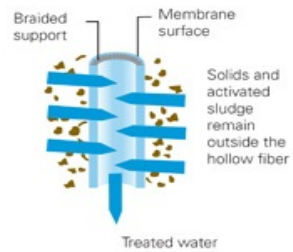
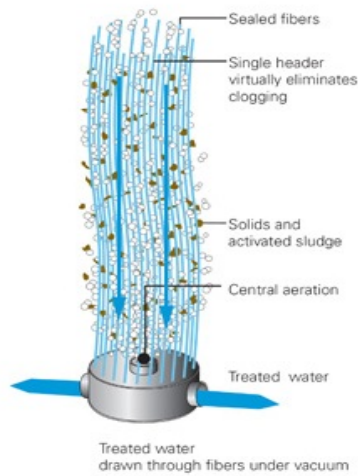
## Desalination







# MEMBRANE APPLICATION



Fuel Cell Technology

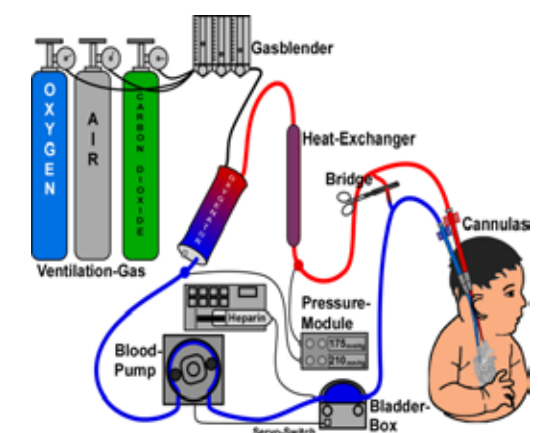
Waste water Treatment

Microreactor (Chemical Industry)

Gas separation

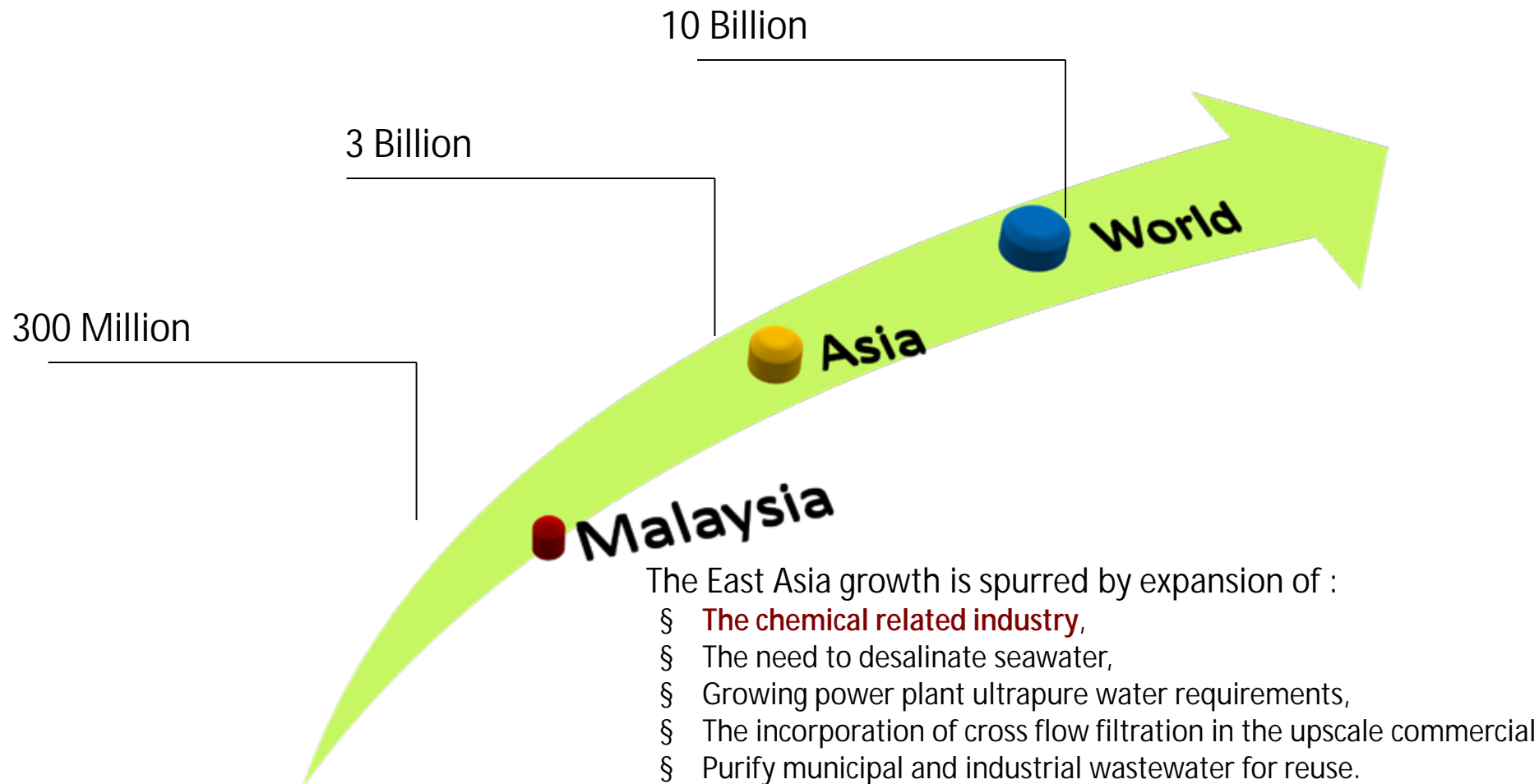
Medicine & Pharmacy

# MEMBRANE APPLICATIONS



Extracorporeal Membrane Oxygenation (ECMO)

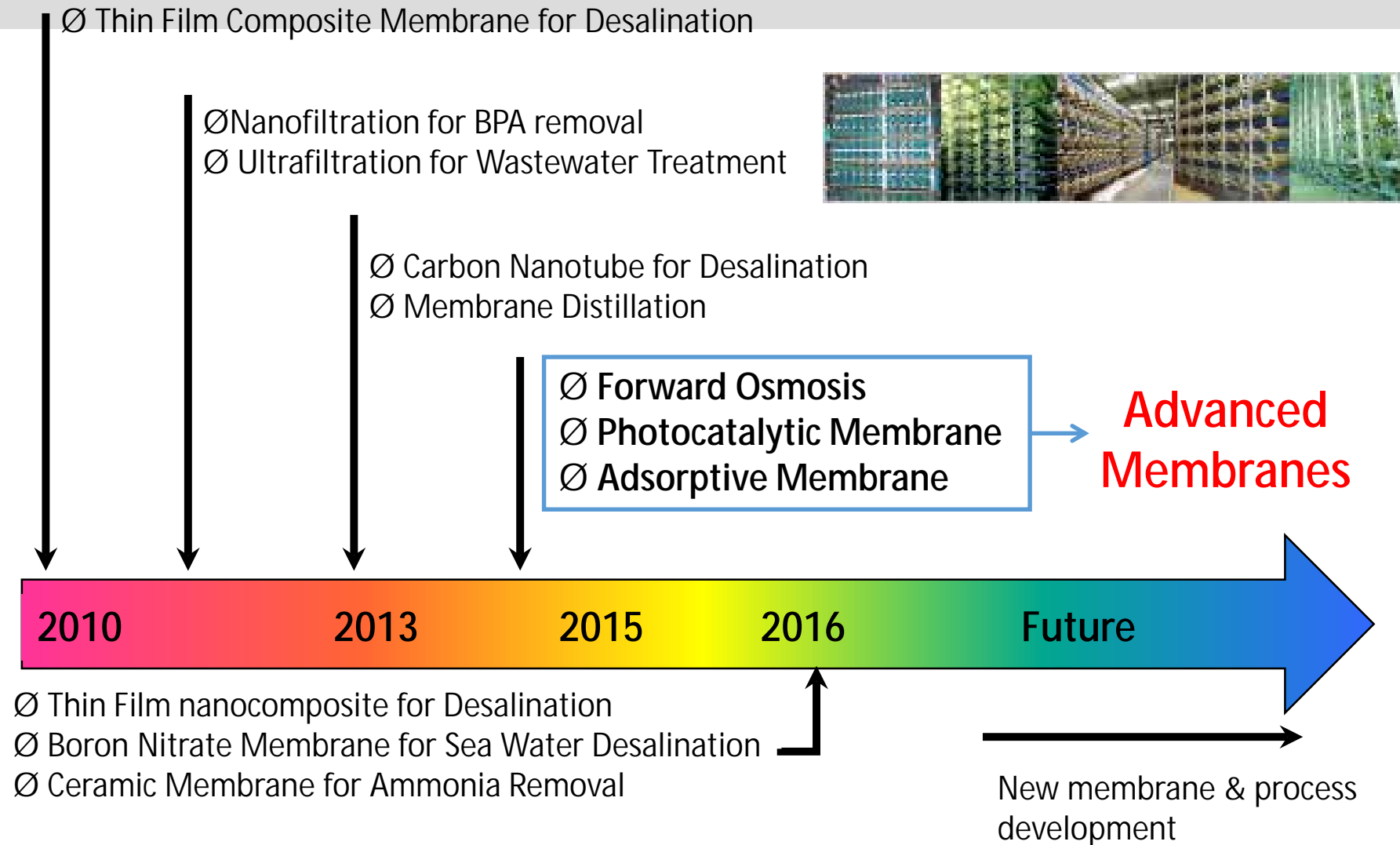
# Projected Demand of Membrane Technology in 2015 (USD)



McIlvaine-Co, 2011



# Membrane Chronological Development

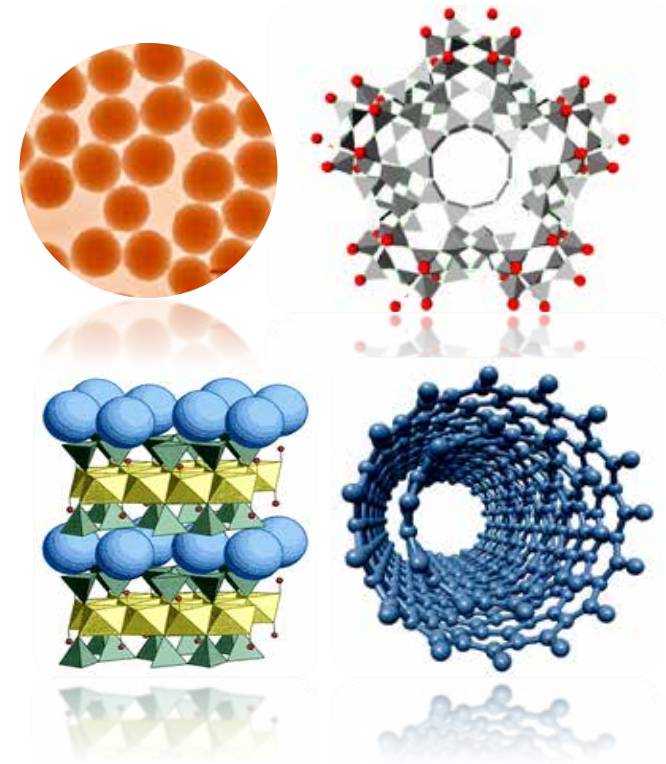




# Nanomaterials in Membrane Technology

# The Next Big Thing: Engineered Nanomaterials

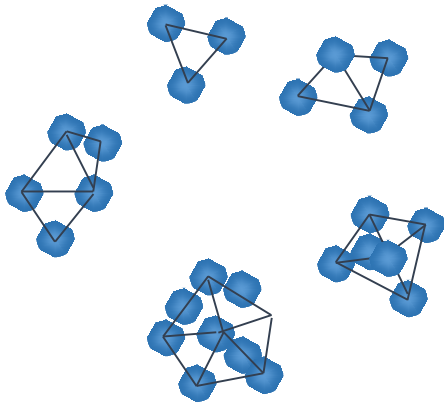
- Nanomaterials are typically defined as materials smaller than 100 nm in at least one dimension.
- At this scale, materials often possess novel size-dependent properties different from their large counterparts.
- Water and wastewater treatment utilize the scalable size-dependent properties of nanomaterials which relate to:
  - High specific surface area and sorption capacity
  - High selectivity and reactivity
  - Fast transport
  - Antimicrobial





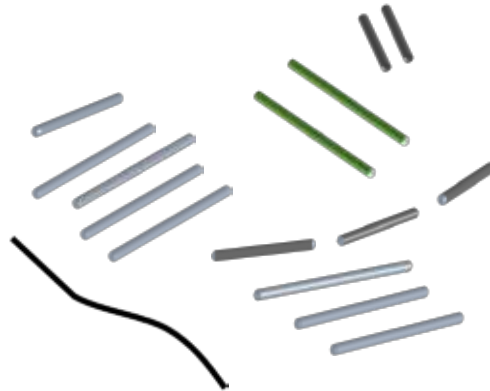
# Classes of Nanomaterials

a) Clusters (0D)



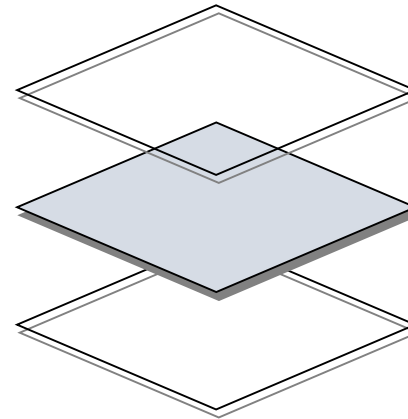
Examples:  $\text{TiO}_2$ ,  $\text{Al}_2\text{O}_3$ ,  $\text{ZrO}_2$ ,  
 $\text{SiO}_2$ ,  $\text{ZnO}$ ,  $\text{Ag}$

b) Nanotubes/rods (1D)



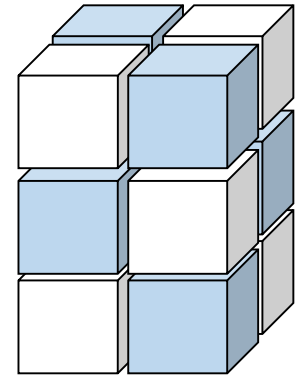
Examples: SWCNTs, MWCNTs,  
titania nanotube

c) Films/ exfoliated (2D)



Examples: graphene, graphene  
oxide, clay silicate

d) Polycrystal (3D)

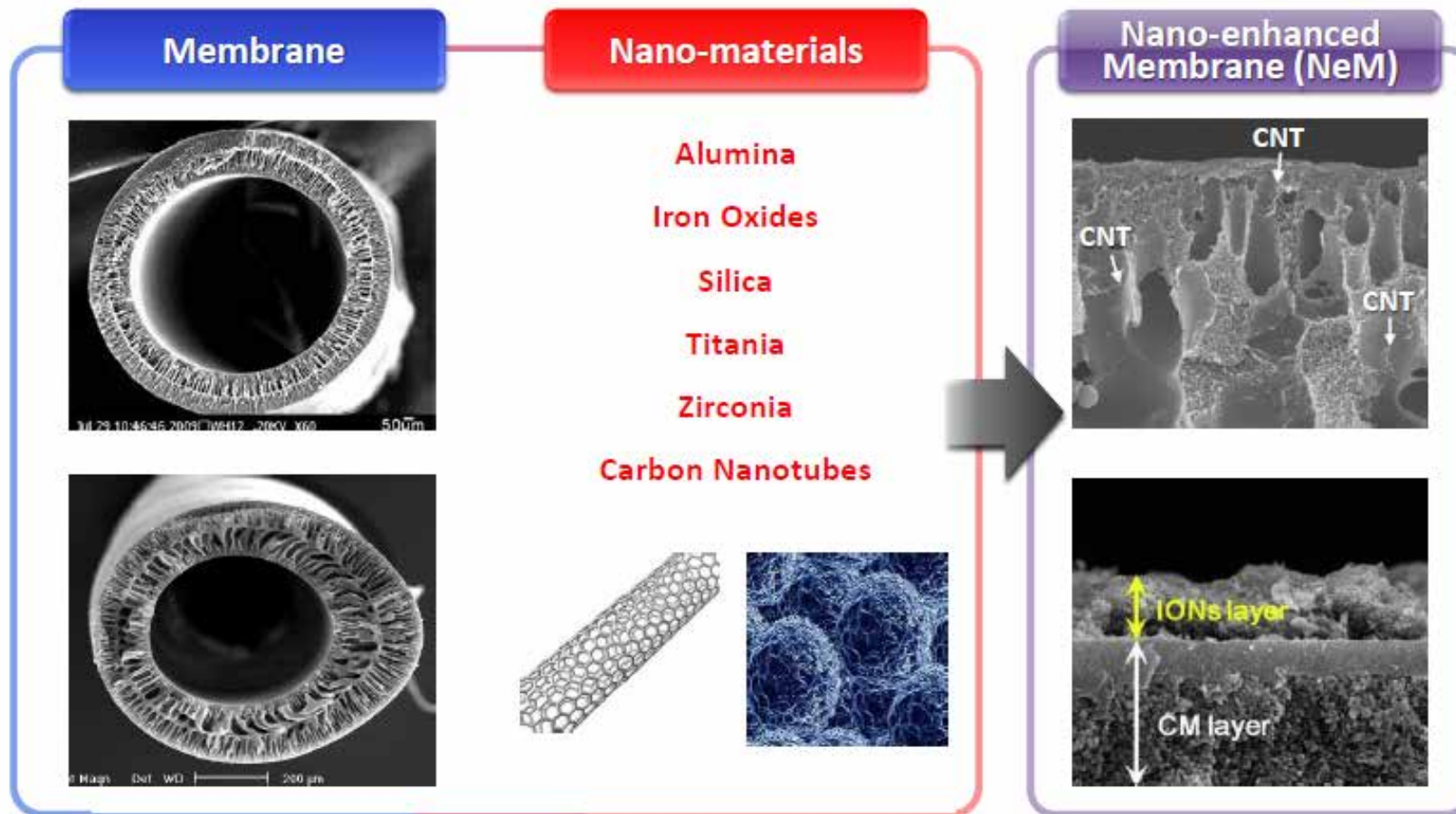


Examples: zeolite, metal  
organic framework

# How Does Nanotechnology Help?

- Recent advances in nanotechnology offer leapfrogging opportunities to develop next-generation water supply systems
- The highly efficient, modular, and multifunctional processes enabled by nanotechnology-provide high performance, affordable and sustainable solutions.
- Less reliance on large infrastructures
- New treatment capabilities that allow economic utilization of unconventional water sources to expand the water supply

# Membrane Enhanced with Emerging Nanomaterials







# Advanced Membrane Technology

- i. Forward osmosis
- ii. Photocatalytic membrane

## (i) FORWARD OSMOSIS-The Principles

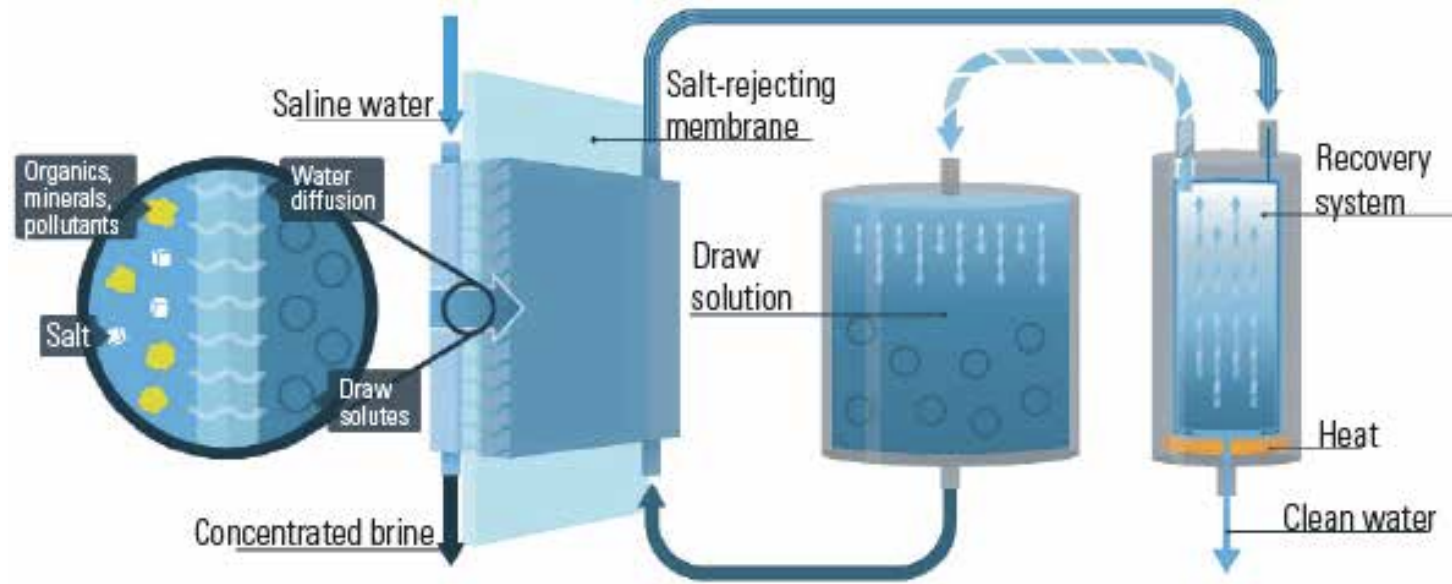


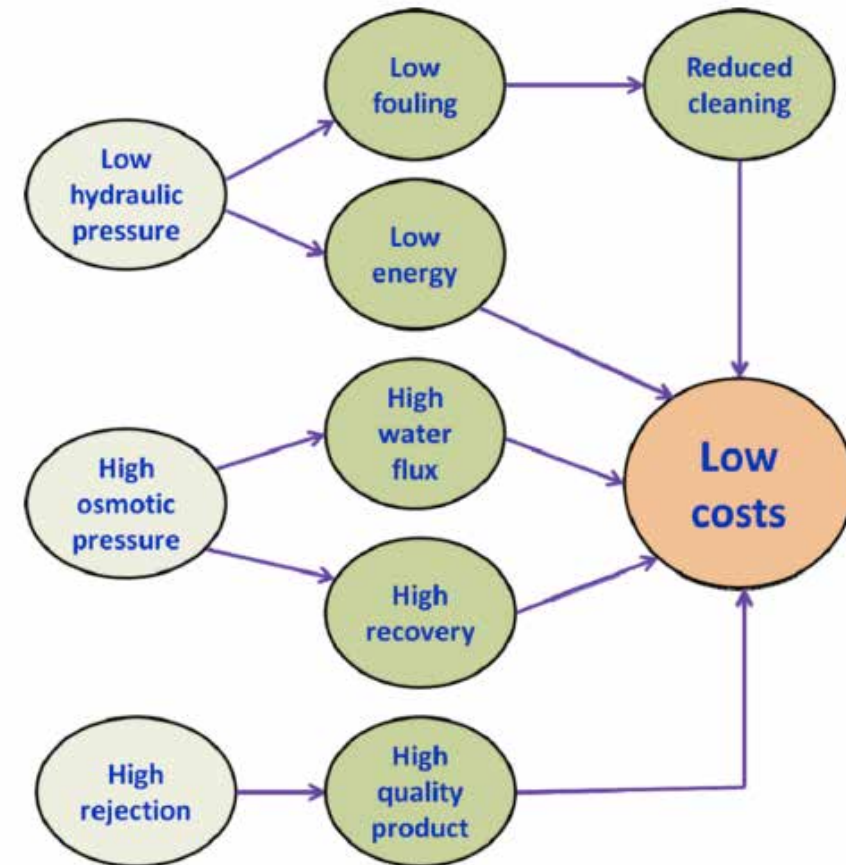
Image: Oasys Water

- FO is an **osmotically driven membrane process** that takes advantage of the osmotic pressure gradient to drive water across the **semipermeable membrane** from the **feed solution** (low osmotic pressure) side to the **draw solution** (high osmotic pressure) side.

# Advantages of FO over Conventional Pressure Driven Membrane Processes

- Due to the very low hydraulic pressure required, FO delivers many potential advantages such as:
  - less energy input
  - lower fouling tendency
  - easier fouling removal
  - higher water recovery

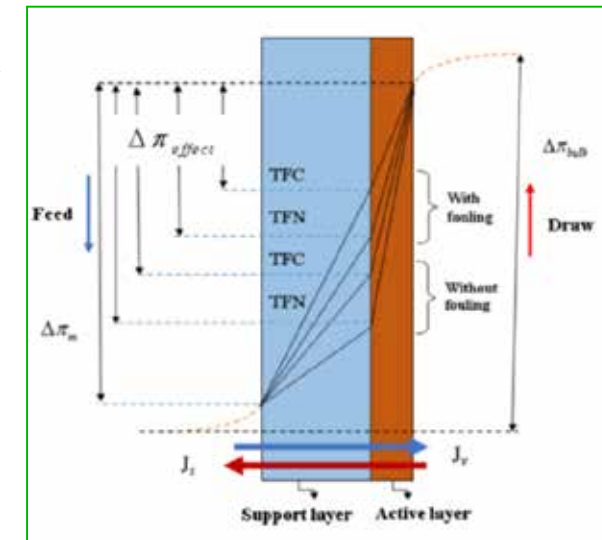
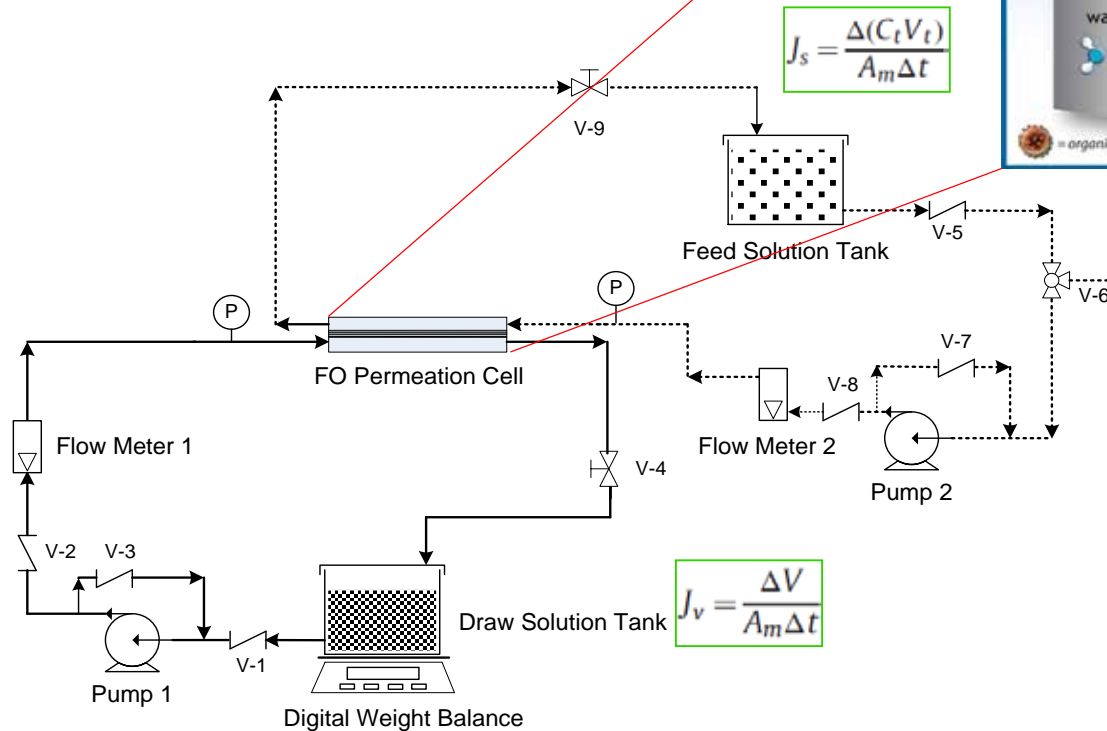
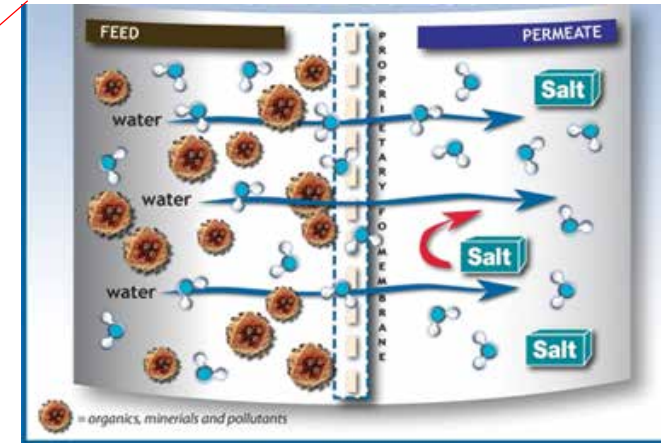
The potential benefits of FO used in water treatment



Zhao et al. Journal of Membrane Science 396 (2012) 1– 21

# FO Membrane Experimental Set-Up

Low osmotic Pressure    High osmotic Pressure



$J_v$ =water permeation flux (based on the volume change in the draw or feed solution)  
 $J_s$ =Salt reverse diffusion flux from the draw solution (based on the conductivity different)

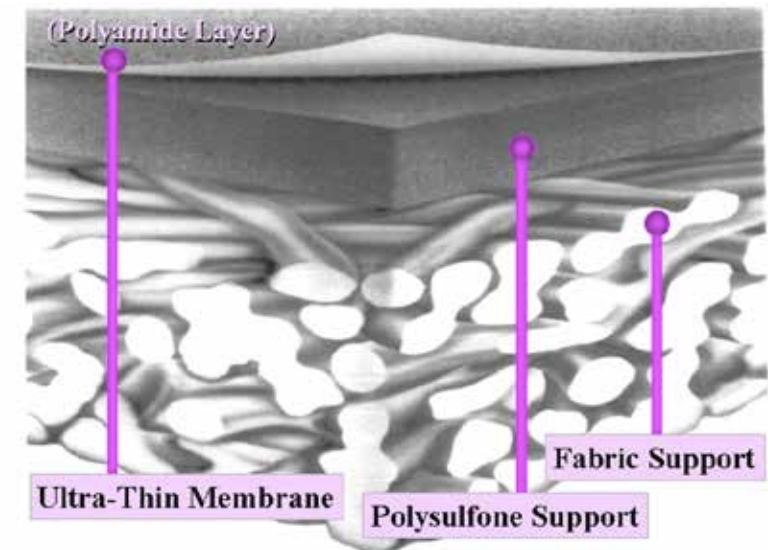
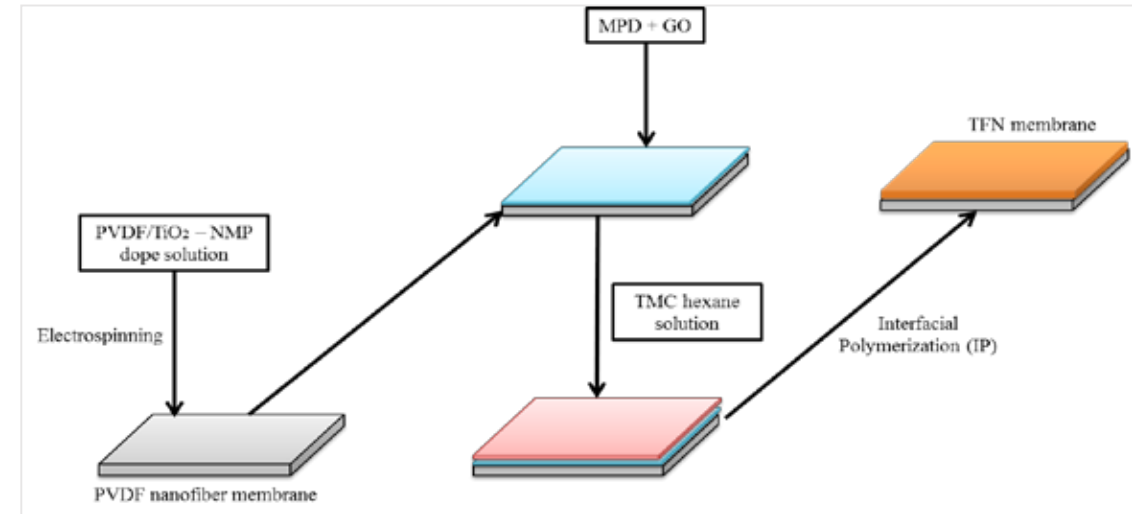


# FO Membrane Characteristics

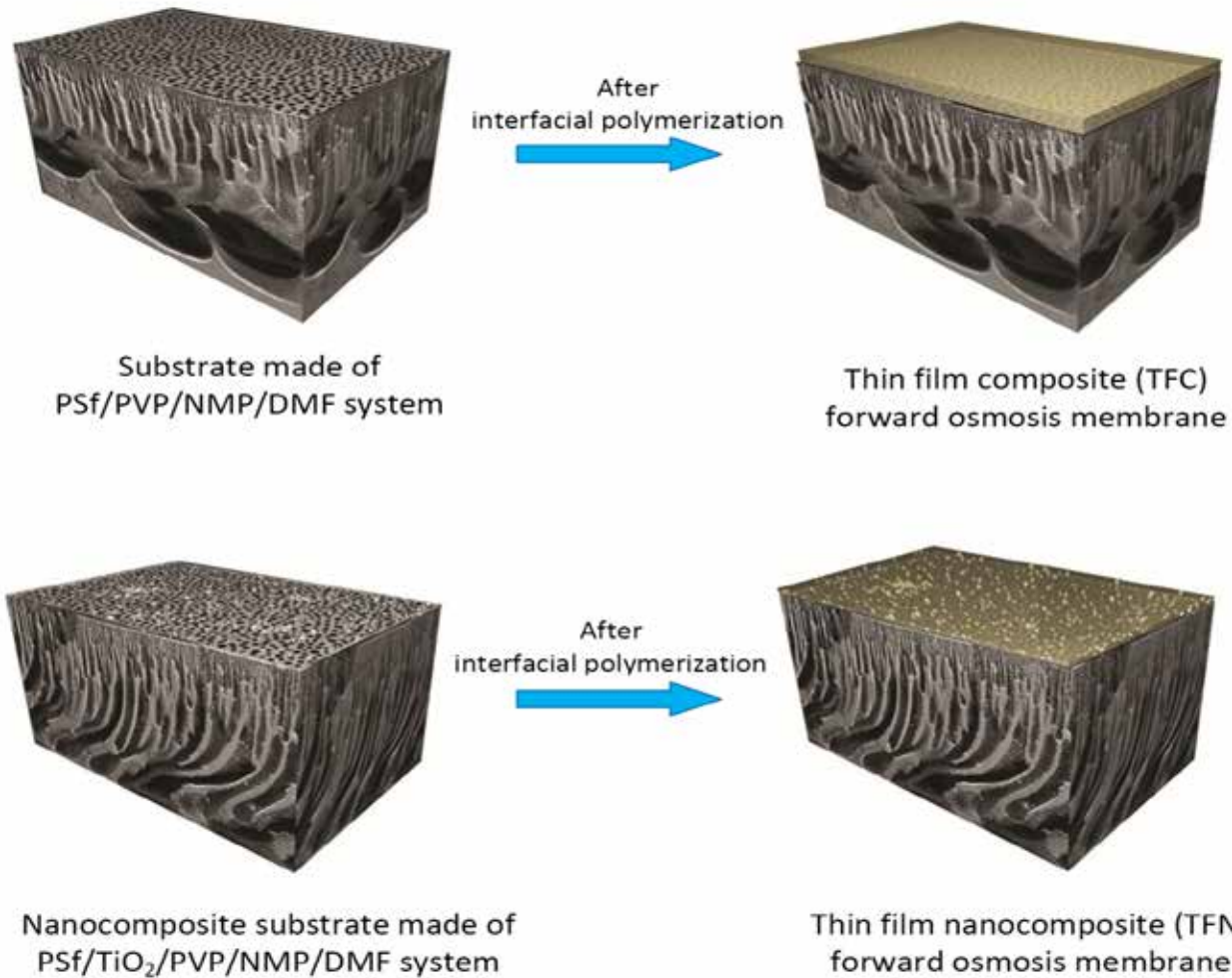
- The polyamide (PA) thin film composite (TFC) (synthesized via interfacial polymerization of MPD (m-phenylenediamine) and TMC(trimesoylchloride), Mitchell et al., 2010) FO membranes are excellent to the existing asymmetric membranes as they exhibit higher water flux and salt rejection.

## The desired characteristics of TFC FO membranes:

- A Thin semi-permeable PA layer free of defects with high water flux and high solute rejection
- A microporous substrate with low ICP
- Highly hydrophilic to improve water flux and antifouling behavior
- High mechanical strength against cleaning and vibration throughout operation

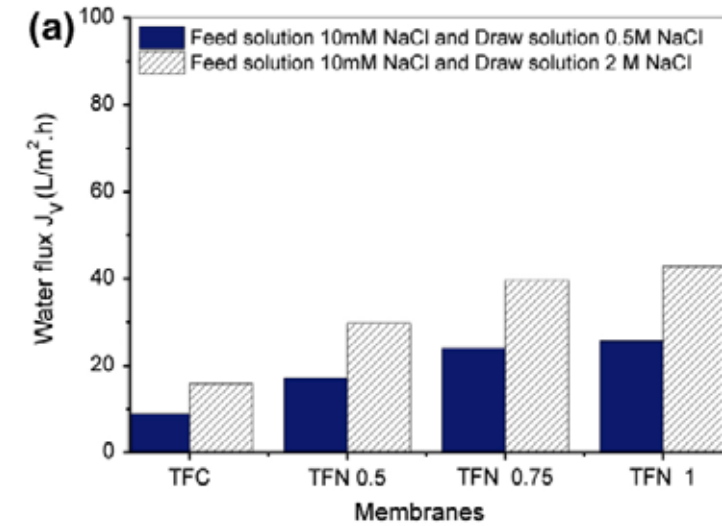
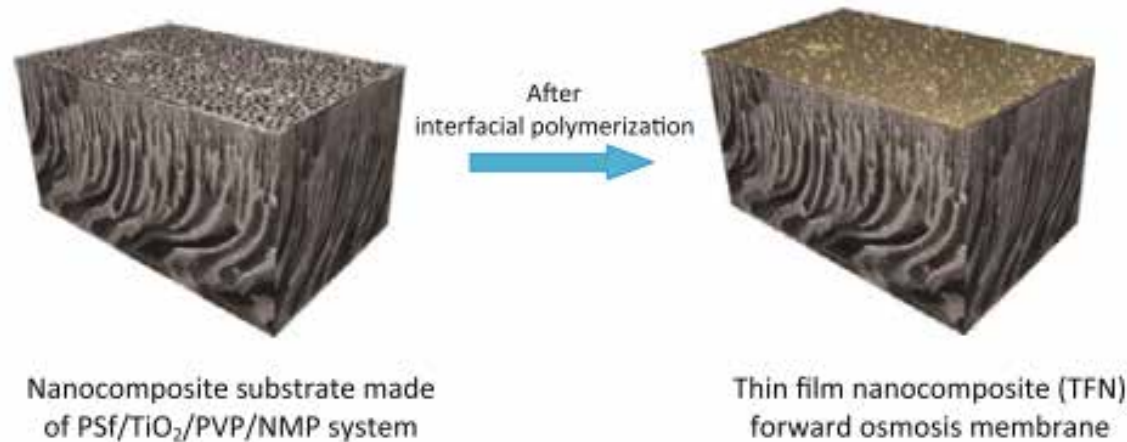


# TFN membrane in FO – the structure



# Thin Film Nanocomposite FO membrane for Desalination

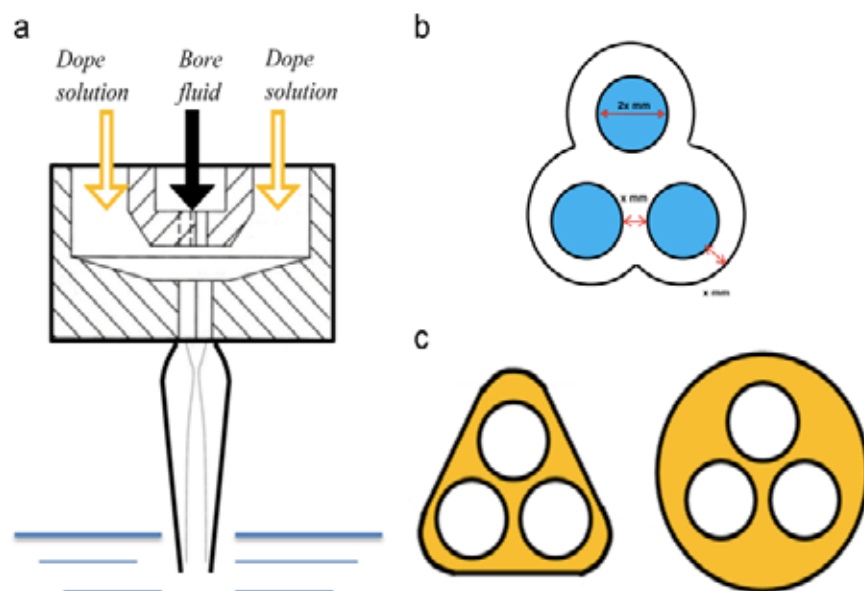
## Polyamide TFN with PSf-TiO<sub>2</sub> nanocomposite substrate



- The hydrophilicity and porosity of the PSf- TiO<sub>2</sub> nanocomposite substrate was improved upon addition of TiO<sub>2</sub>.
- The increase in water permeability can be attributed to decrease in structural parameter which resulted in decreased internal concentration polarization (ICP).

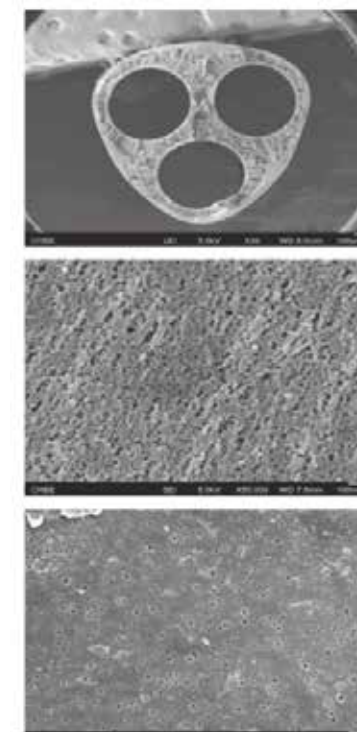
# Hollow Fiber FO membrane for Desalination

## Tri-bore hollow fiber membrane



(A) Single layer tri-needle spinneret; (B) bottom view of the tri-needle spinneret; (C) cross sections of as-spun tri-bore HFs.

- The triangle TFC-FO membrane exhibits improved water permeability than the round one. The TFC-triangle FO membrane has the highest water fluxes of 11.8 LMH with low salt reverse fluxes of 2.5 gMH FO modes.
- In addition, much more fibers can be packed in a FO module if TFC tri-bore HF membranes have a triangle shape instead of a round one.





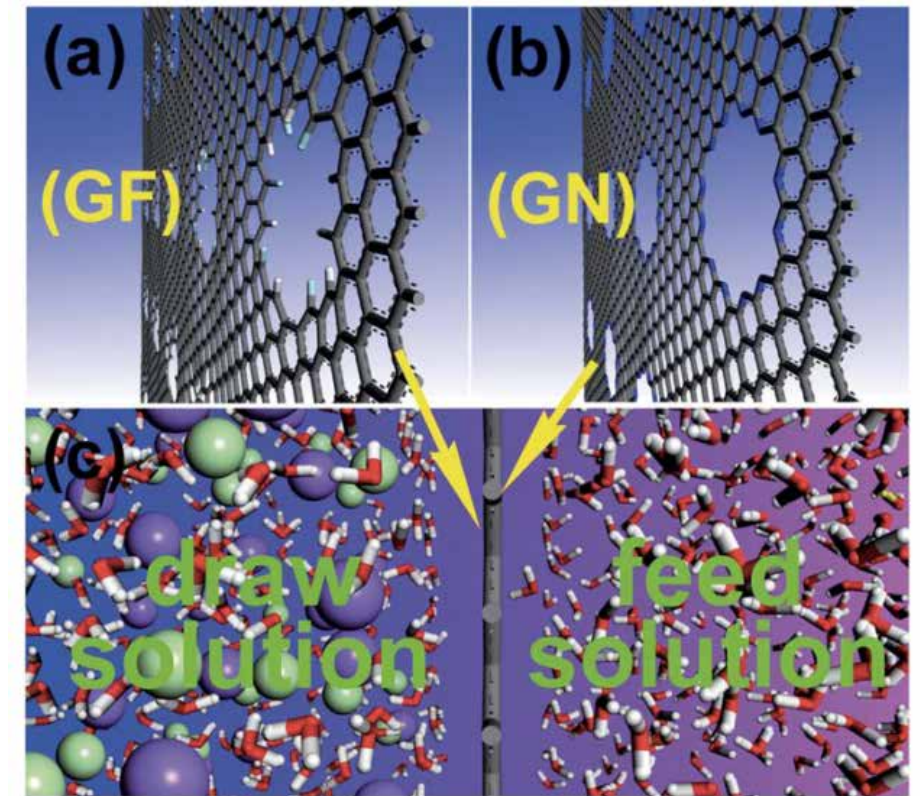
# Graphene FO Membrane For Desalination-Molecular Dynamic Simulation

- Porous graphene can be used as an FO membrane without the requirement of a support layer. Hence exhibits zero Internal Concentration Polarization (ICP) if external hydraulic pressure is not necessary.
- The dangling bonds in the graphene pores can be saturated with N or F atoms to form functional graphene monolayers:
  - Fluorinated porous graphene (GF)
  - Nitriding porous graphene (GN)

**TUNABLE PORE PROPERTIES**-The flux and rejection can be tuned by the presence of F and N:

With N atom-**water flux decreases** and **salt rejection increases** (due to stronger attractions between membrane pores and solutions)

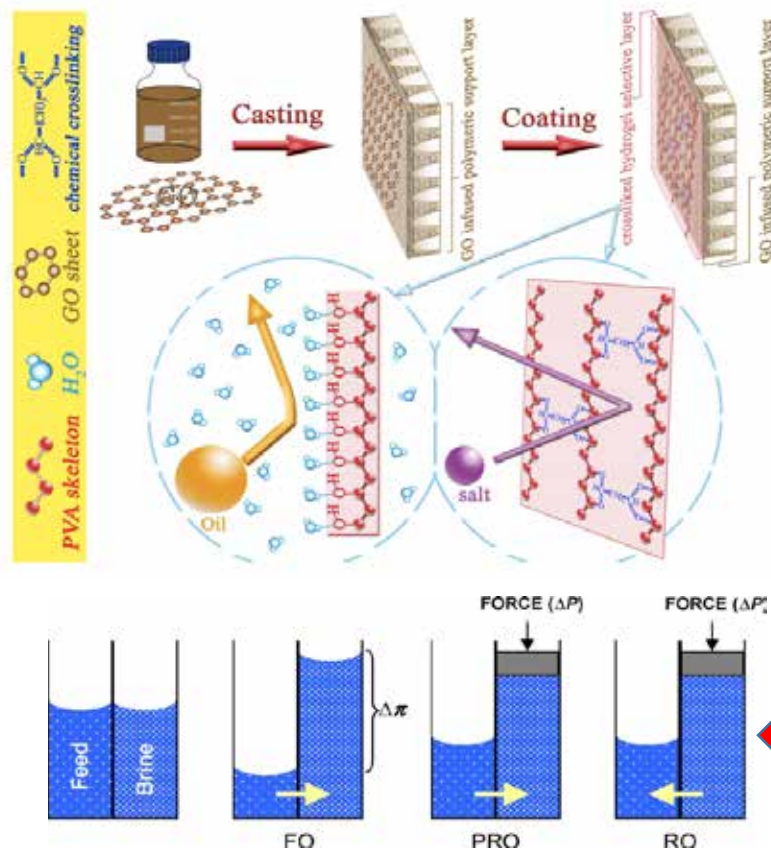
With F atom-**ultrafast water flux** due to less adsorption energy compared to N atoms.



Gai et al. J. Mater. Chem. A, 2014, 2, 4023

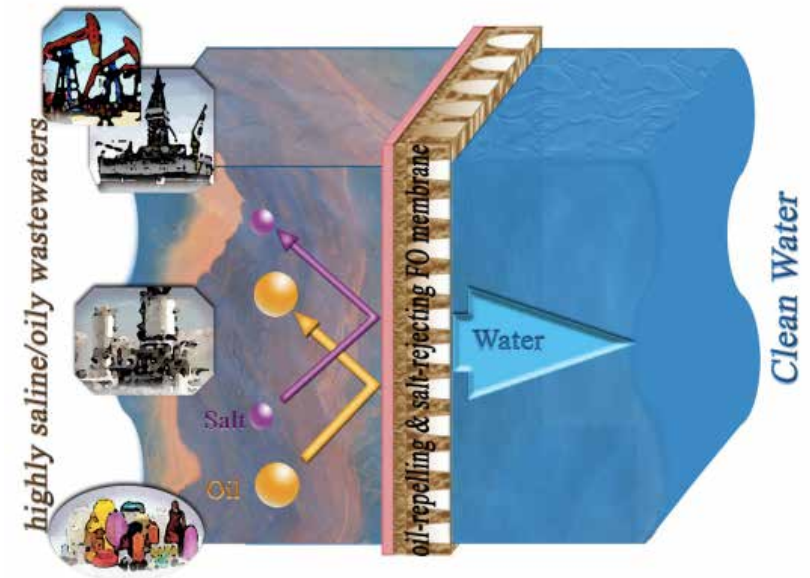
# Nanocomposite FO membrane for Shale Gas (Highly Saline oil) Wastewater Treatment

Nanocomposite FO membrane composed of an oil-repelling and salt rejecting hydrogel selective layer on top of a graphene oxide (GO) nanosheets infused polymeric support layer for **simultaneous oil-repellency and salt-rejection**



Parameters and intrinsic properties accountable for S value determination:

- The pure water membrane permeability coefficient (A)
- The salt permeability coefficient (B)
- The water flux  $J_w$  – **IN FO MODE** – at a given osmotic driving force

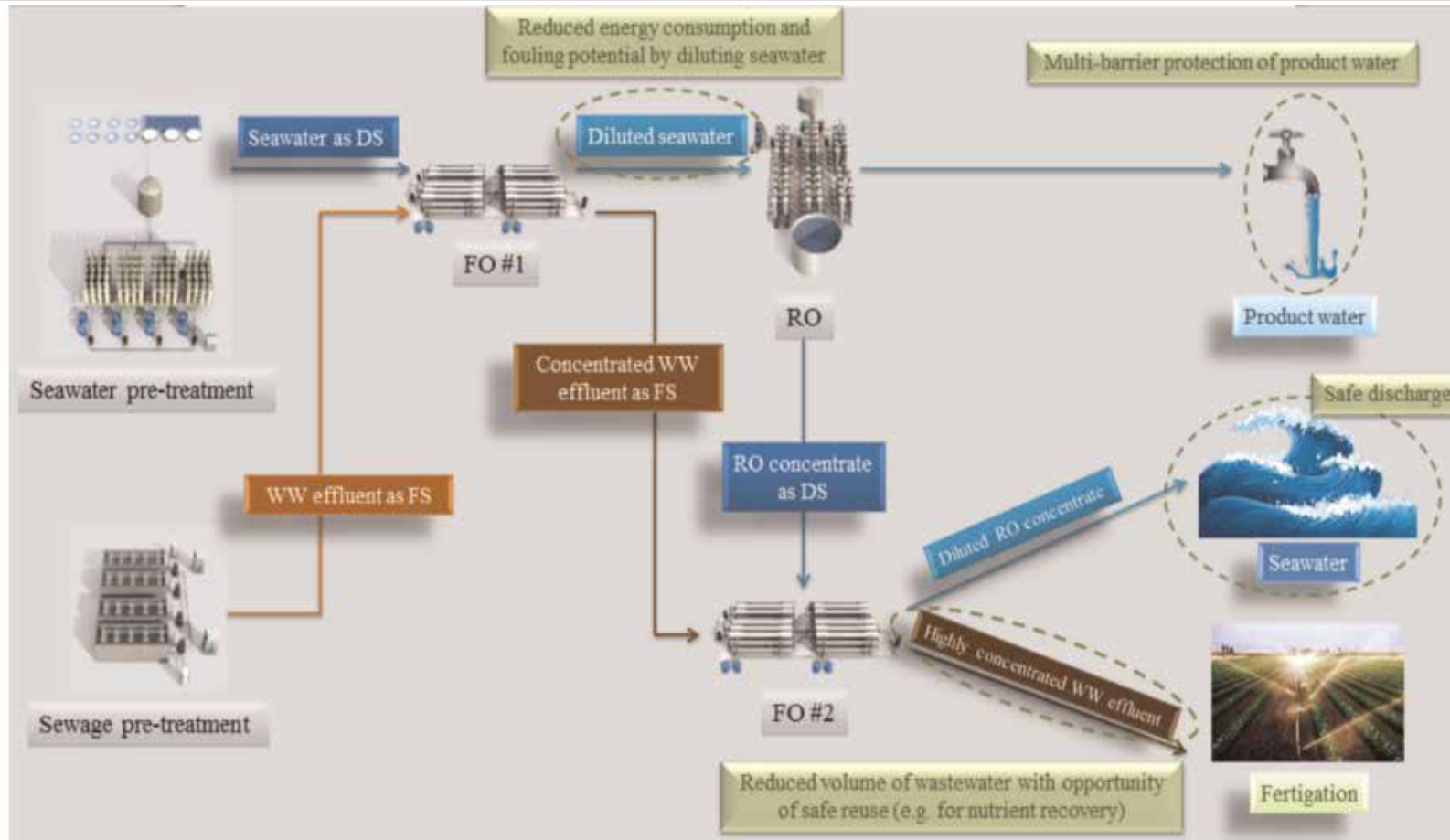


The synthesized FO membranes possess ultrahigh rejections of multivalent inorganic ions as well as emulsified oils.

The infused GO nanosheet plays a crucial role to improve FO membrane structure (reducing structural parameter, S value=resistance of membrane's support layer towards solute diffusion) by reducing the tortuosity as well as increasing the porosity of the support layer, and consequently lead to constantly high water flux

Qin et al. Nature Scientific Reports 5, Article number: 14530 (2015)

# FO-RO hybrid system



Schematic of an FO–RO hybrid process plant for simultaneous treatment of wastewater and seawater desalination (DS: draw solution; FS: feed solution; RO: reverse osmosis; WW: wastewater)



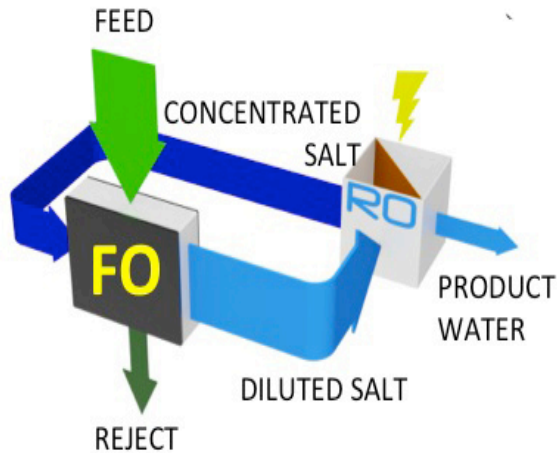
# Hybrid FO System for Desalination

FO acts as pretreatment in conventional desalination

## FO + RO

- Produces high quality water
- Uses simple salt as a draw
- FO is low fouling and provides nano-level pre-treatment for RO

### 1. FO as pre-treatment for RO

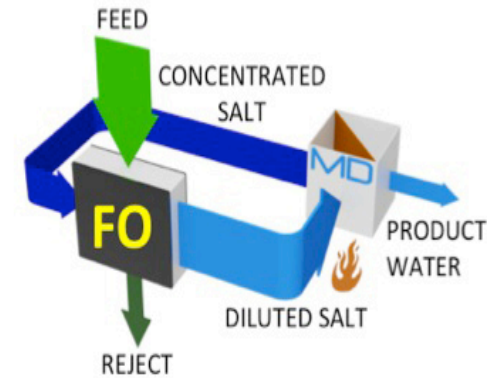


## FO + Thermal Draw Recovery

- Efficient if waste heat is available

### 2. FO + Membrane Distillation (MD)

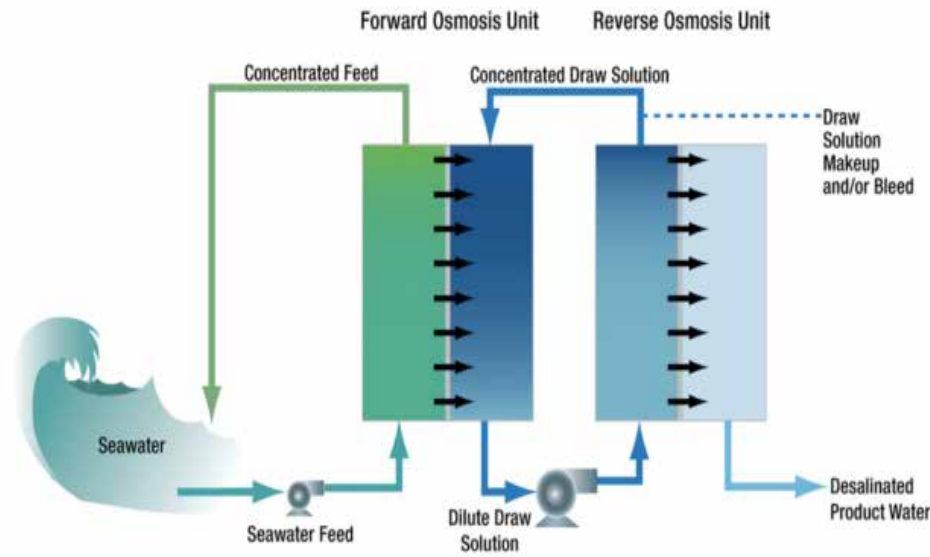
- Uses simple salt as a draw
- FO reduces fouling of MD



Images: International Forward Osmosis Association

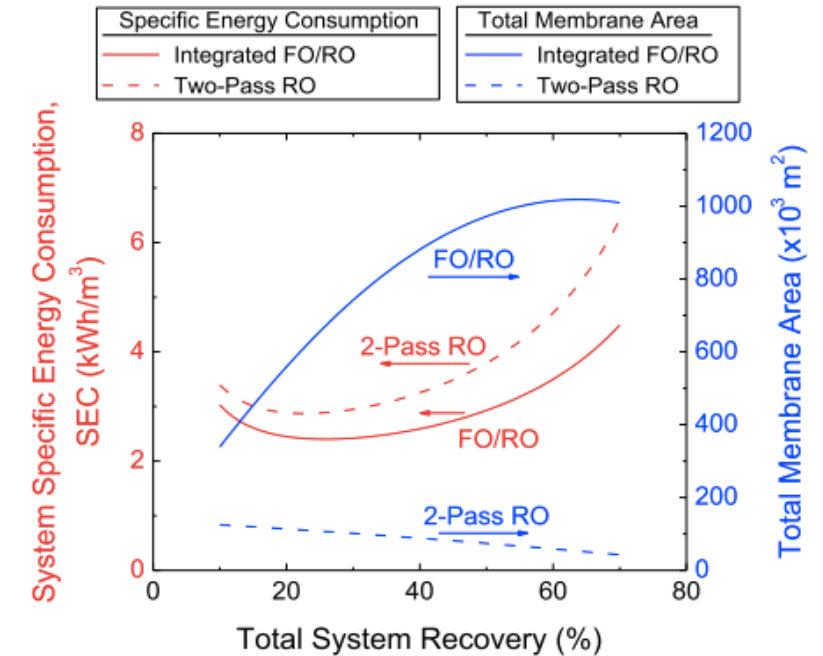


# FO-RO Desalination



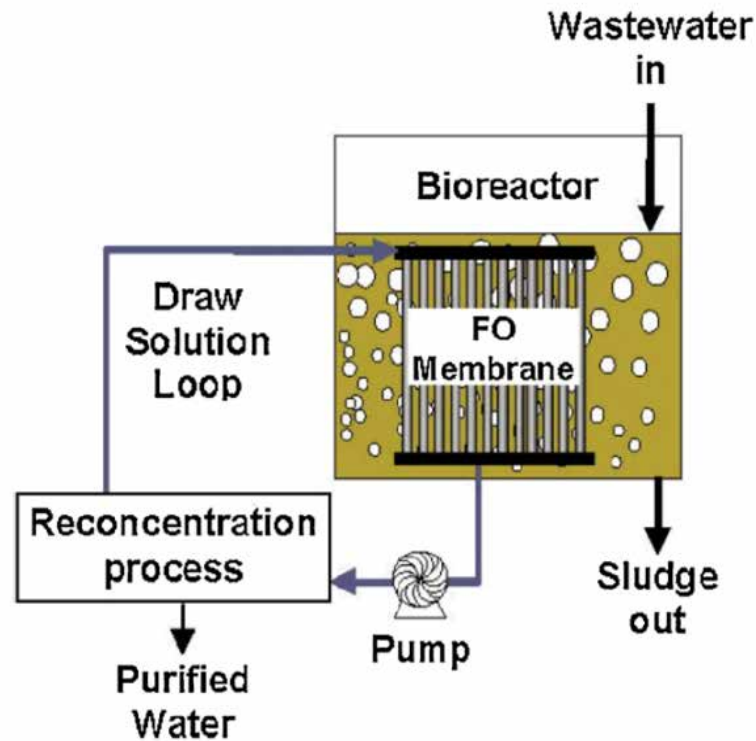
The key benefits include

- (i) Energy saving
- (ii) chemical storage and feed systems may be reduced for capital and operations and maintenance cost savings,
- (iii) water quality is improved for increased consumer confidence and reduced process piping costs
- (iv) the overall sustainability of the desalination process is improved.



Specific energy consumption (SEC) and total membrane area of an integrated FO-RO seawater desalination process compared to a two-pass RO process.

# FO for Osmotic Membrane Bioreactor (OMBR)



Compared to seawater, general wastewater has lower osmotic pressure but much higher fouling propensity. Low fouling tendency is one of the most pronounced advantages of FO.

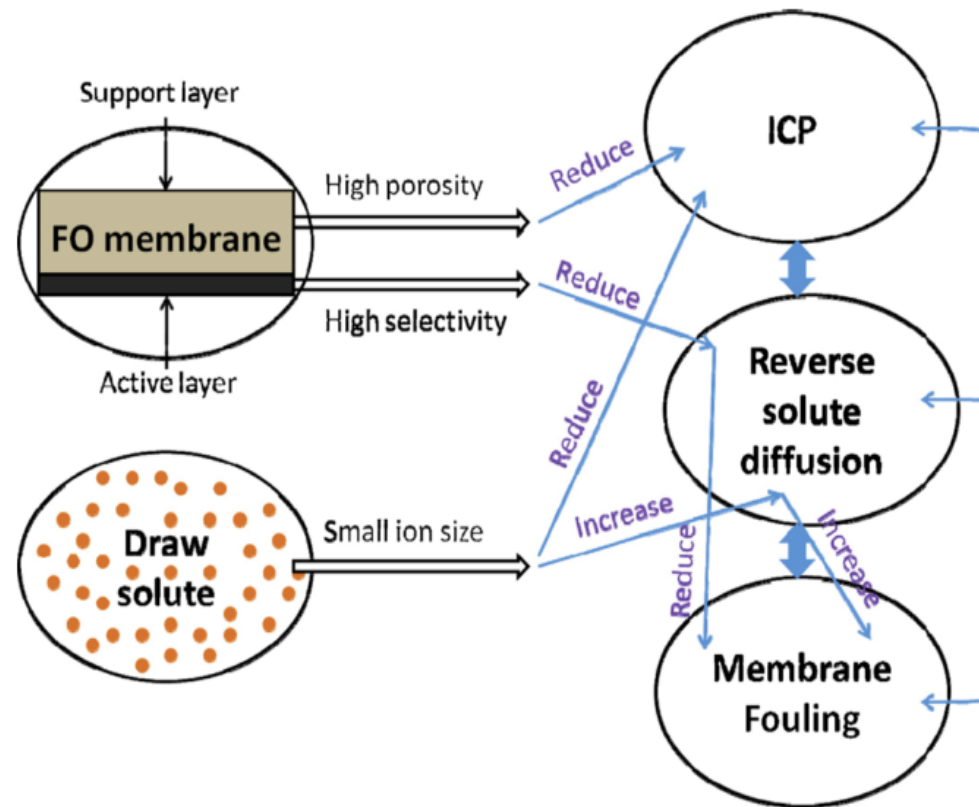
The ratio of the membrane salt permeability ( $B$ ) to the water permeability ( $A$ ) (i.e.  $B/A$ ) and the ratio of hydraulic retention time (HRT) to sludge retention time (SRT) (i.e.  $HRT/SRT$ ) are two important parameters for the optimization of OMBR operation.

To minimize the flux decline caused by salt accumulation, these two ratios should be low

# Challenges of FO for Water Reclamation

1. Concentration polarization
2. Membrane fouling
3. Reverse solute diffusion
4. The need for membrane development
5. The design of the draw solute

Relationships between ICP, membrane fouling, reverse solution diffusion, membrane characteristics and draw solute properties in FO



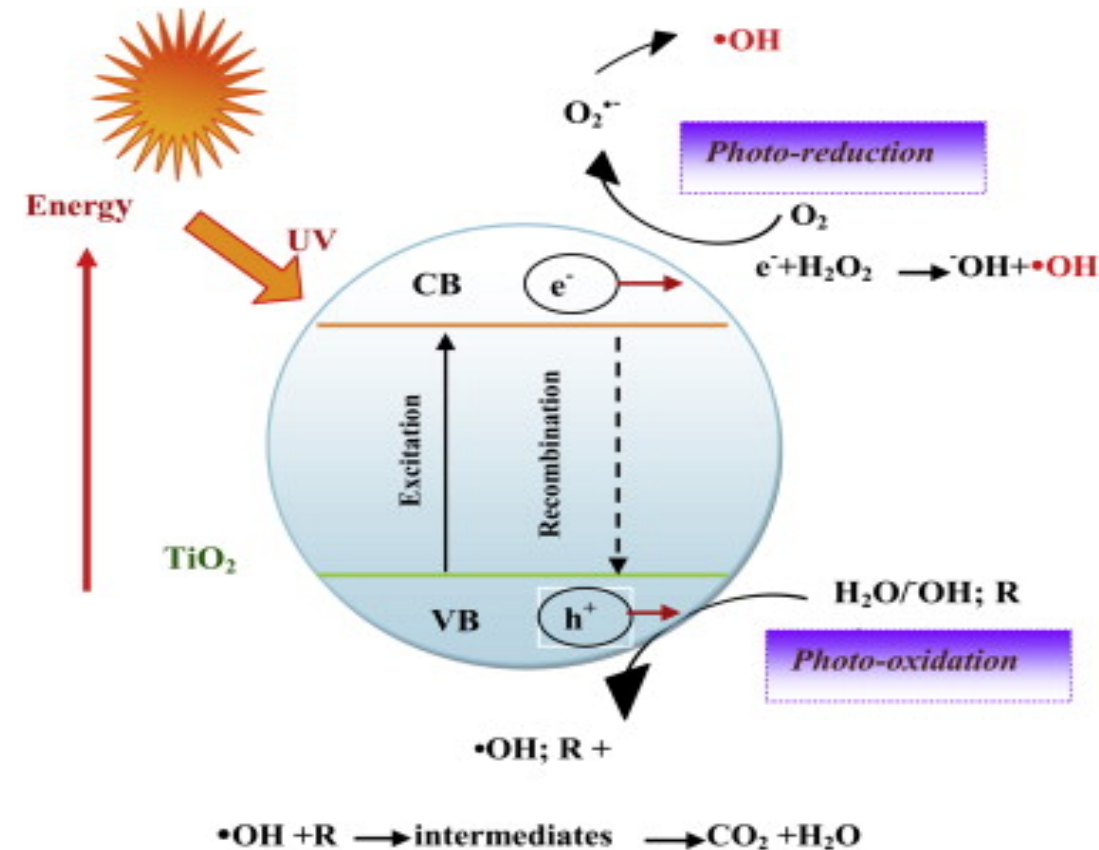
## (ii) Photocatalysis

Photocatalysis is the acceleration of chemical reaction based on the OH<sup>-</sup> generation, induced by the absorption of light by a catalyst (TiO<sub>2</sub>; remarkable charge transfer property and oxidation ability). One of its application is to treat the organic pollutant in water.

- Two types of photocatalytic reactors:
1. Separated photocatalysis and separation chamber
  2. Hybrid chamber

Advantages:

1. Reaction and separation occurred simultaneously
2. Eliminate separation step for catalyst

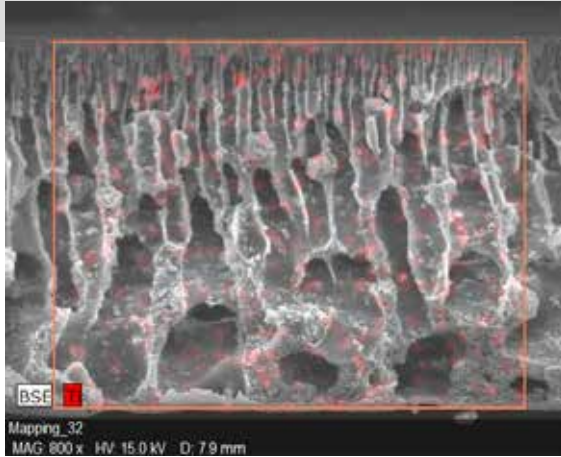


CB- Conductance band  
VB- Valence band

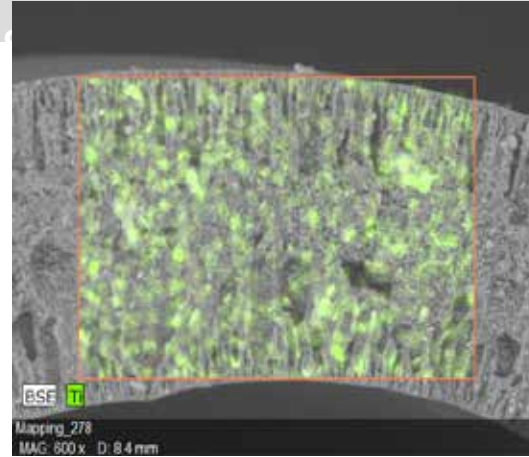


# Type of Photocatalytic Membranes

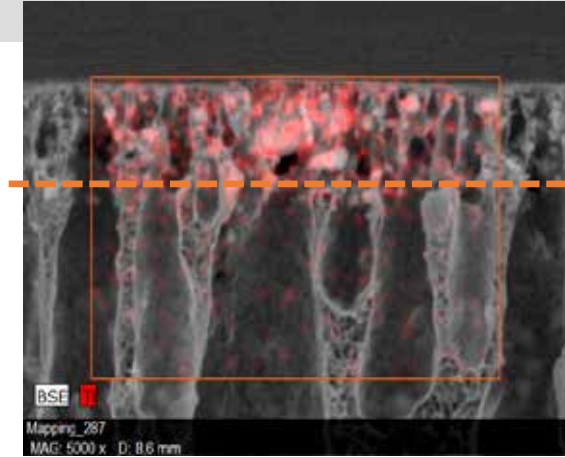
Cross-section



Flat sheet membrane

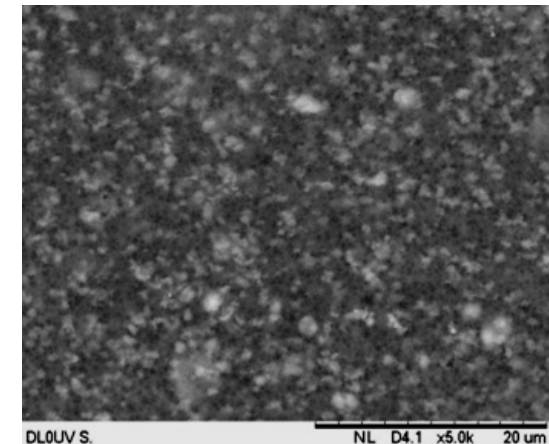
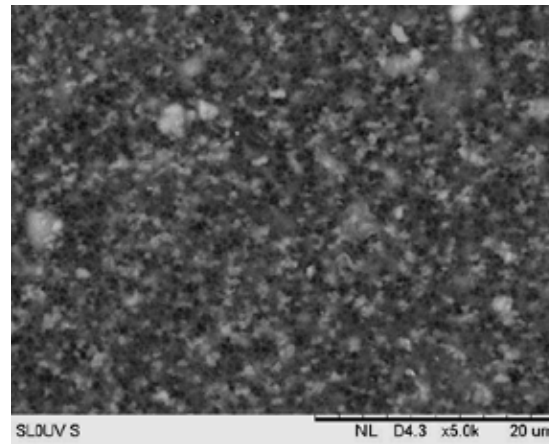
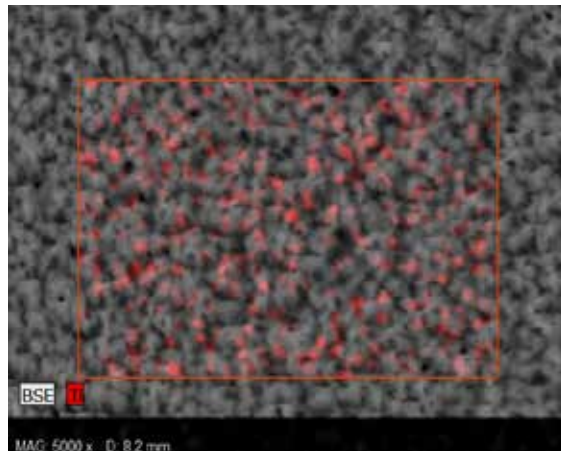


Single layer hollow fibre



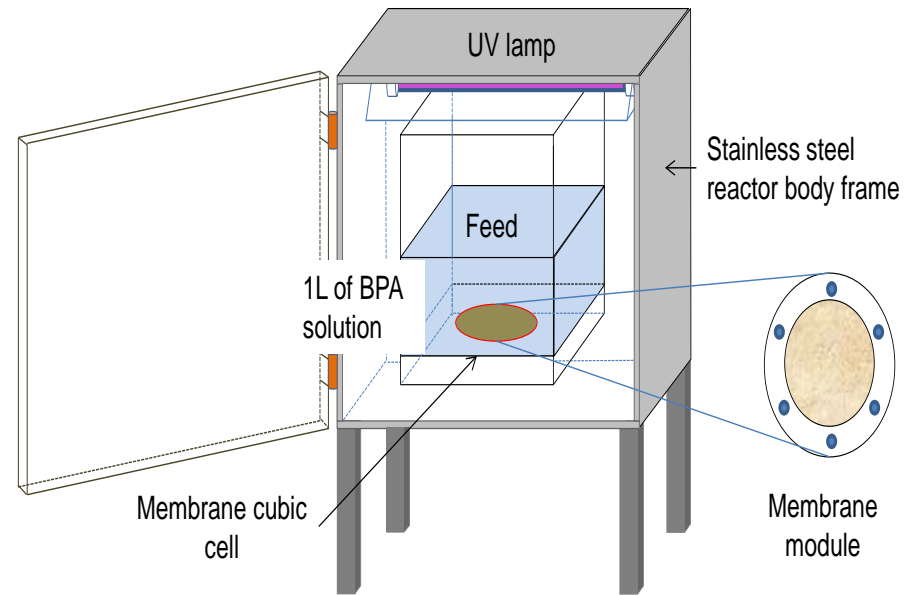
Dual layer hollow fibre

Membrane surface

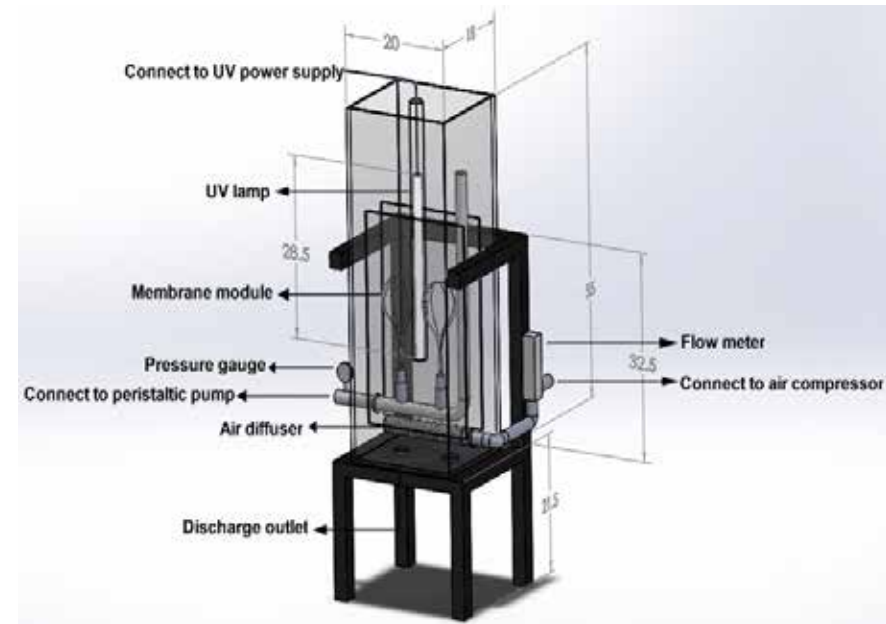


# Photocatalytic Membrane Reactor

Membrane: Flat sheet membrane  
Pollutant: Biphenol A (BPA)

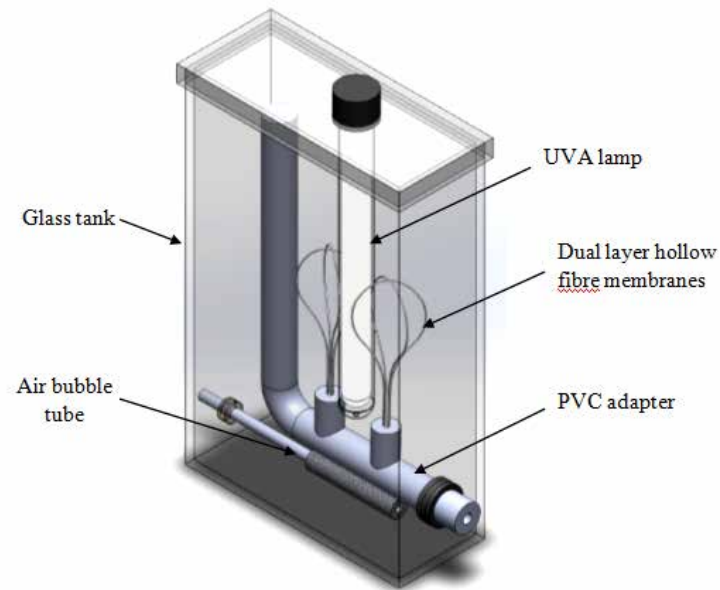


Membrane: Single layer hollow fiber membrane  
Pollutant: Oily wastewater

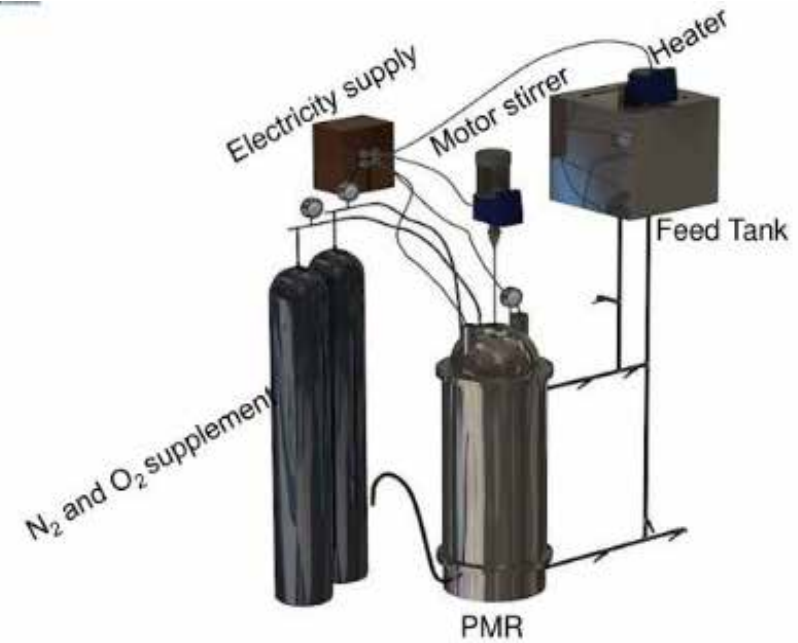


# Photocatalytic Membrane Reactor

Membrane: Dual layer hollow fiber membrane  
Pollutant: Nonylphenol (NP)



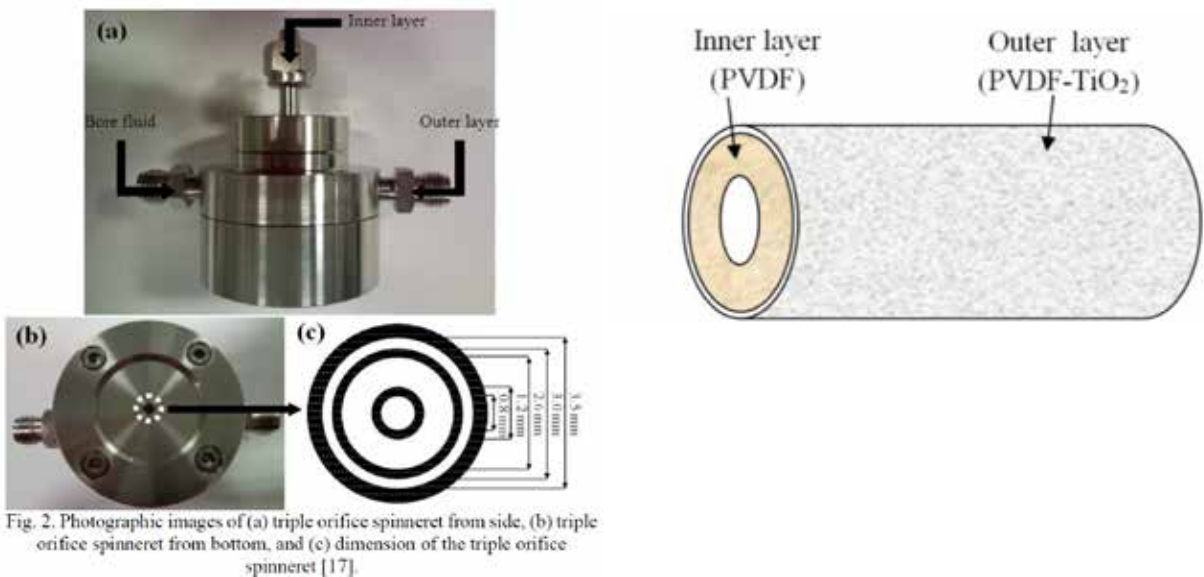
Membrane: Flat sheet / Hollow fiber membrane  
Pollutant: Oily wastewater



# PHOTOCATALYTIC DUAL LAYER HOLLOW FIBRE MEMBRANES FOR NONYLPHENOL DEGRADATION

- ü Distribution of  $\text{TiO}_2$  nanoparticles within membrane is a crucial part of this process because much of the reaction relies on the performance of the catalyst.
- ü Via co-spinning process (involves 2 different phase inversion pathways simultaneously), dual-layer hollow fibre membrane with  $\text{TiO}_2$  distributed onto selected outer layer can be produced.

Comparison of single and dual layer hollow fibres' properties (ratio  $\text{TiO}_2/\text{PVDF}$ : 0.5)

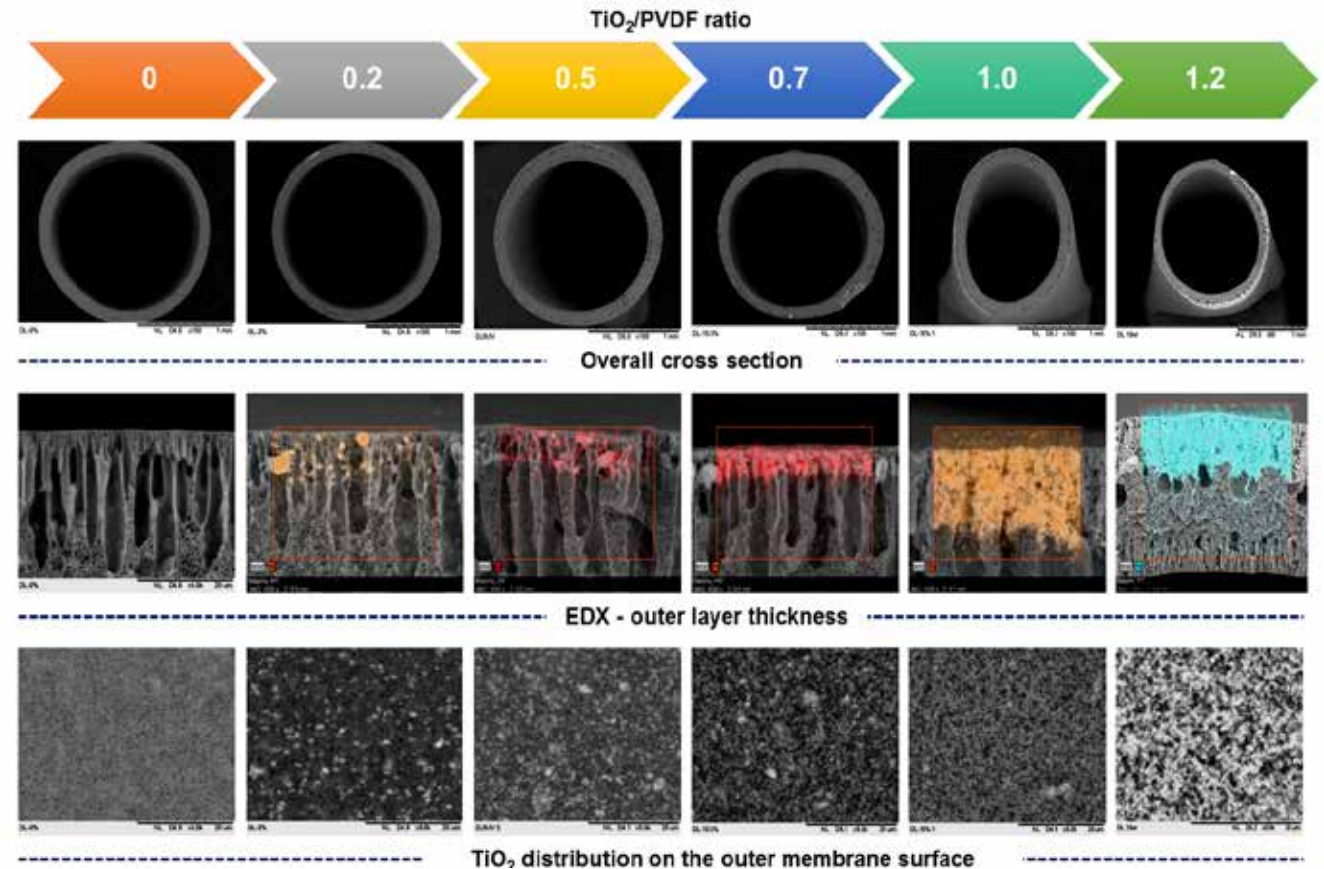


Properties	Single layer	Dual layer
$\text{TiO}_2$ distribution		
Contact angle	84.0 °	77.6 °
Nonylphenol degradation	70%	85%



# PHOTOCATALYTIC DUAL LAYER HOLLOW FIBRE: Effect of Different Loadings of TiO<sub>2</sub> on Membrane Structures

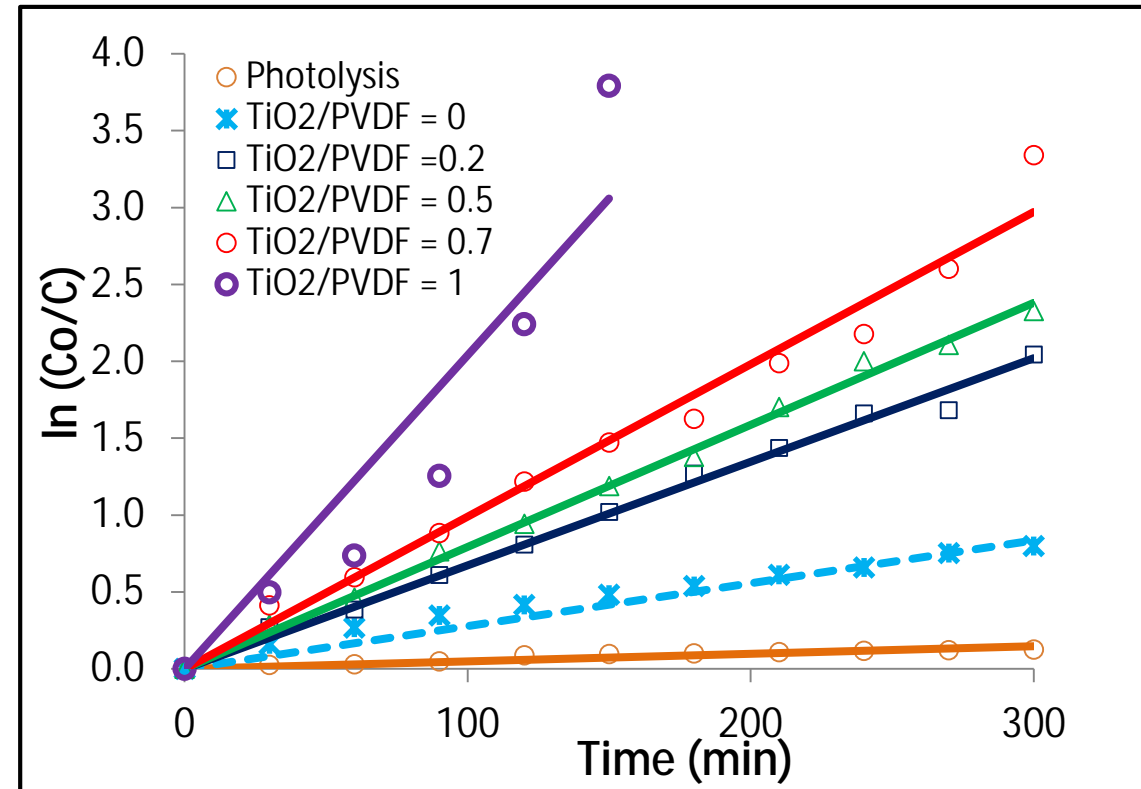
- § Hollow fibres with TiO<sub>2</sub>/PVDF ratio of 0 to 1.2 were developed via co-spinning process
- § Inner layer consisted of 100% PVDF, while outer layer was a mixture of TiO<sub>2</sub>/PVDF
- § Thickness of outer layer varied with the loading, the higher the loading, the thicker the thickness
- § Good adhesion between inner and outer layers can be achieved even for very high loading of TiO<sub>2</sub>



A.F. Ismail et al., Journal of Membrane Science 479 (2015) 123-131

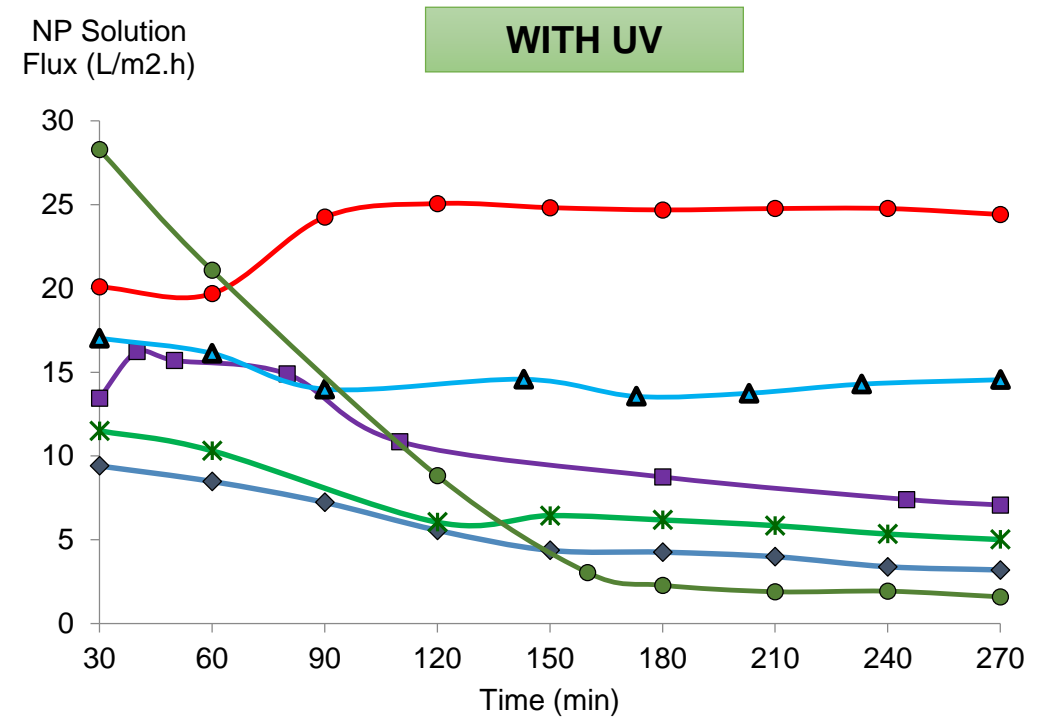
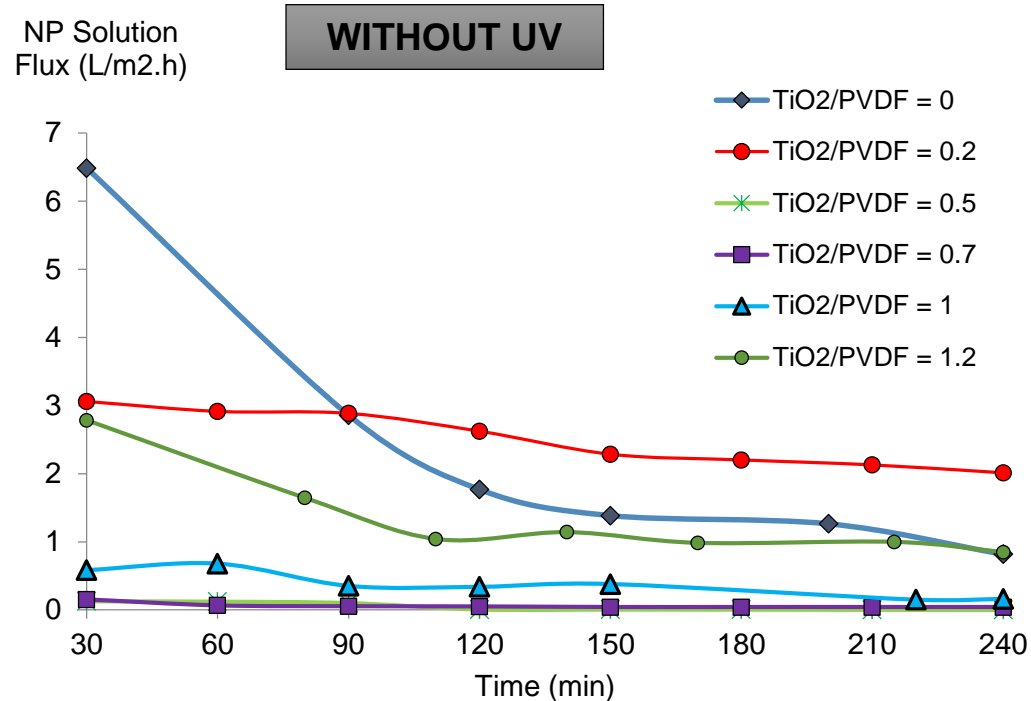
# PHOTOCATALYTIC DUAL LAYER HOLLOW FIBRE: Effect of Different Loadings of $\text{TiO}_2$ on Nonylphenol Degradation

- No degradation occurs under photolysis conditions
- The photocatalytic degradation of NP did not occur since no catalyst was immobilized on the membrane.
- The degradation activity which represented by kinetic showed a significant increase when  $\text{TiO}_2$  loading was increased.
- Achieved the fastest degradation for the membrane with the highest  $\text{TiO}_2$  loading.



Degradation kinetics of NP using different ratio of  $\text{TiO}_2/\text{PVDF}$  membrane

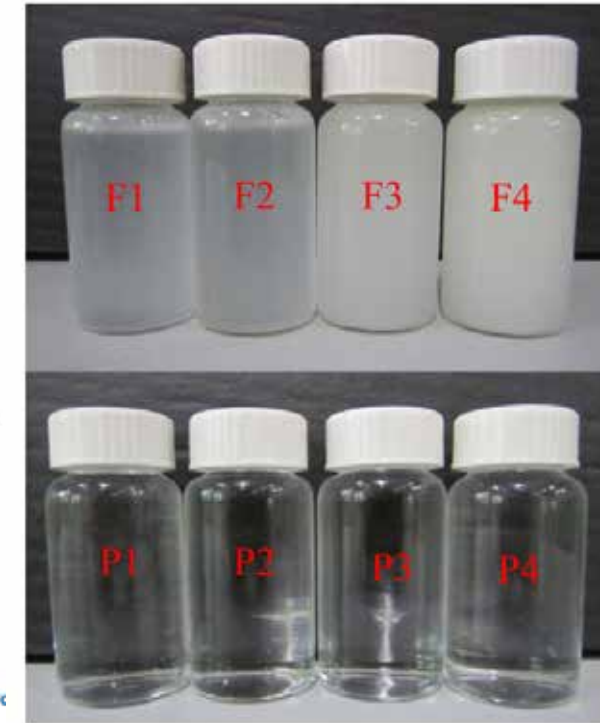
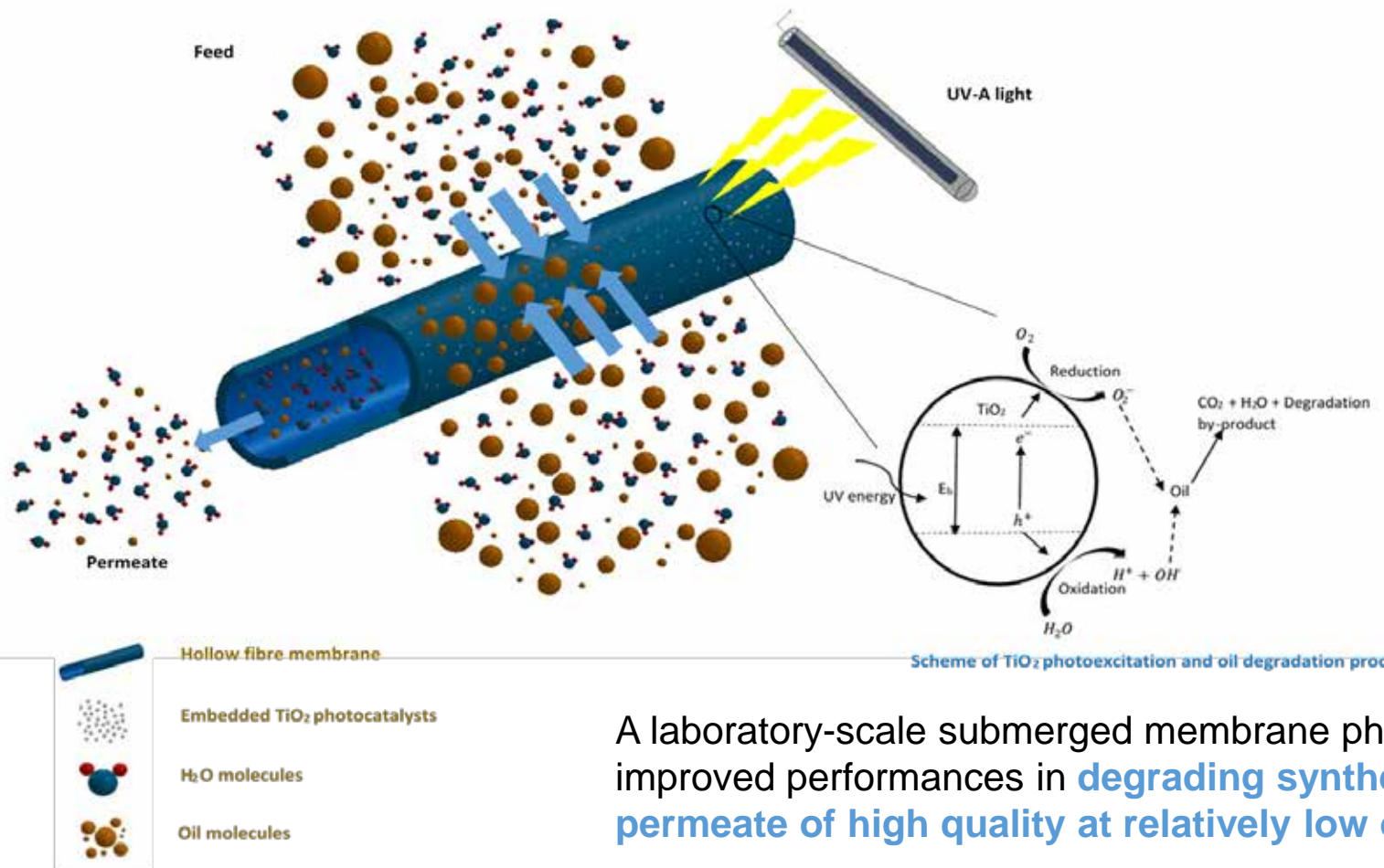
# PHOTOCATALYTIC DUAL LAYER HOLLOW FIBRE: Effect of Different Loadings of $\text{TiO}_2$ on Filtration Performance



ü  $\text{TiO}_2$  may partially prevent the decline of permeate flux and allow to reach a higher stabilized flux more rapidly than without UV irradiation.

ü **0.2  $\text{TiO}_2/\text{PVDF}$**  ratio shows an **optimum value** for NP flux compared to other, it may due to the **distribution of  $\text{TiO}_2$  nanoparticles** at the outer layer in DLHF membranes.

# PHOTOCATALYTIC MEMBRANE FOR OILY WASTEWATER TREATMENT



FEED with different concentration of cutting oil

PERMEATE with clear solution that comply discharge standard

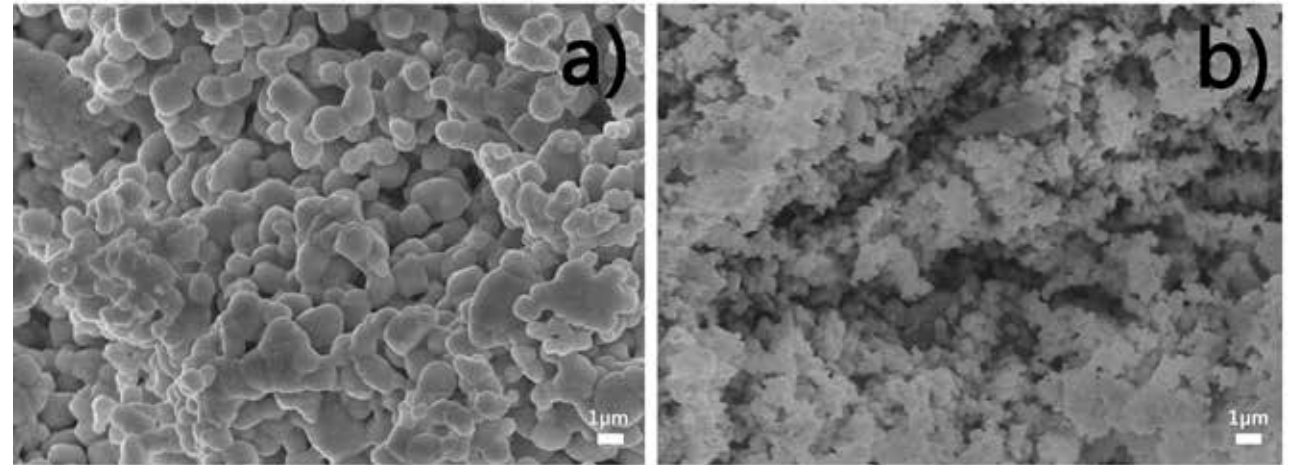
A laboratory-scale submerged membrane photocatalytic reactor (sMPR) exhibited remarkably improved performances in **degrading synthetic cutting oil wastewater** and producing **permeate of high quality at relatively low operating cost**.

C.S. Ong, W.J. Lau, P.S. Goh, A.F. Ismail et al Desalination 353 (2014) 48–56



# Current Challenges of Photocatalytic Membrane

- § Tendency for nanoparticle photocatalyst agglomeration at high loading → reduce photocatalytic activity performance, mechanical strength
- § High operation cost due to high UV light's power consumption
- § Instable PVDF as base membrane when exposure to UV at long term

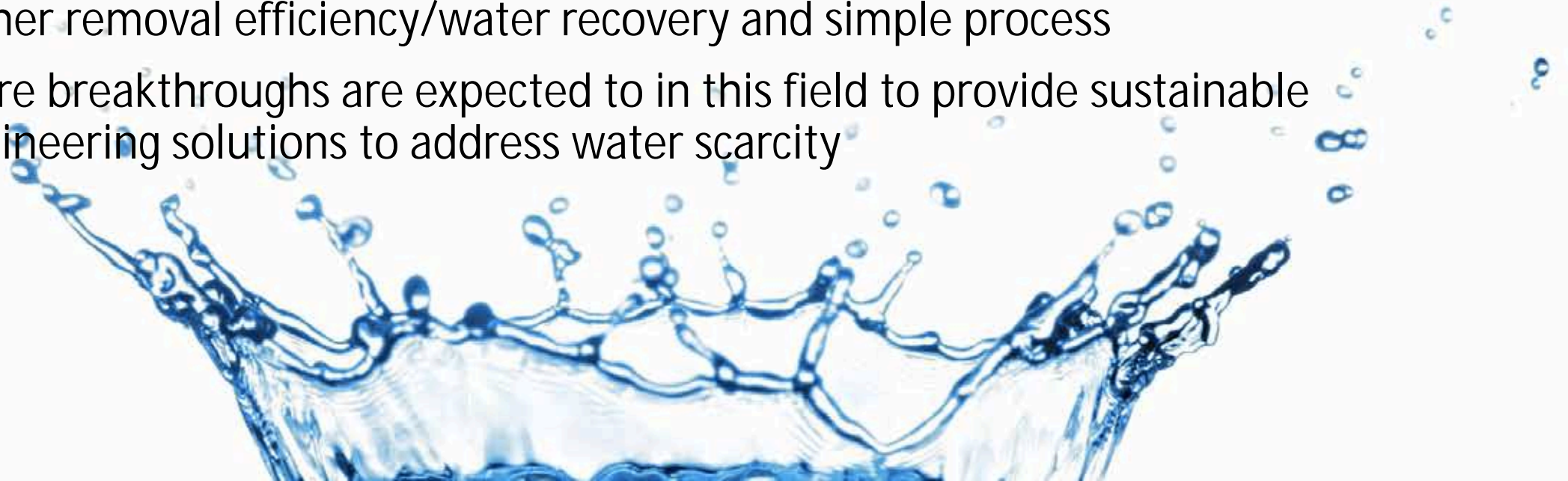


## Way forward of Photocatalytic Membranes

- § Co-spinning is able to reduce the effect of nanoparticle agglomeration
- § Shifting from UV-driven to visible light driven photocatalyst
- § The use of robust ceramic membrane to replace polymeric membrane

## 5. Concluding Remarks

- Membrane technology provides engineering solution for water shortage through water reclamation (wastewater treatment and desalination)
- The application of nanomaterials have further heightened the performances of membrane technology
- Emerging advanced membrane processes offered Lower energy consumption, higher removal efficiency/water recovery and simple process
- More breakthroughs are expected to in this field to provide sustainable engineering solutions to address water scarcity



# Acknowledgement

§ Members and students of AMTEC, UTM

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§ Ministry of Education Malaysia

§ Ministry of Science, Technology and Innovation Malaysia



# Community Services

## Community Service to Supply Drinkable Water at Kiulu, Sabah (2017)

- Ø The portable drinking water filtration system has been developed by AMTEC, UTM to provides clean and safe drinking water to community in Kampung Rumindako Kiulu, Tamparuli, Sabah
- Ø Water resource that is used for the treatment of process water is obtained from **ground water**
- Ø The system capable to supply 2000 Liter per day of which can cater around 1000 peoples.





# Community Services

## Community Service for Flood Relief at Kelantan (2016)

- Ø The integrated mobile reverse osmosis (RO) water purification system (UTM Membrane) is developed by AMTEC, UTM.
- Ø Water resources that are used for the treatment of process water is obtained from **river water, tube well and seawater**.
- Ø To provide **quality water support to small units** where the distribution of water is not feasible during the occurrence of natural disaster.
- Ø The system provides clean water support **without committing large water production assets** from the logistics support structure.
- Ø The system tailors water production capacity to fulfil the demands of independent **Special Operations Forces, detachments** and units typically engaged in **remote site missions**.





# Community Services

## Earth Quake Relief at Ranau, Sabah (August 2015)





# Community Services

## Flood Relief at Pekan, Pahang (Jan 2015)



# Community Services

## Pantai Senok Desalination Plant (2017)

Site: Kampung Pantai Senok, Kelantan  
(Private Land)

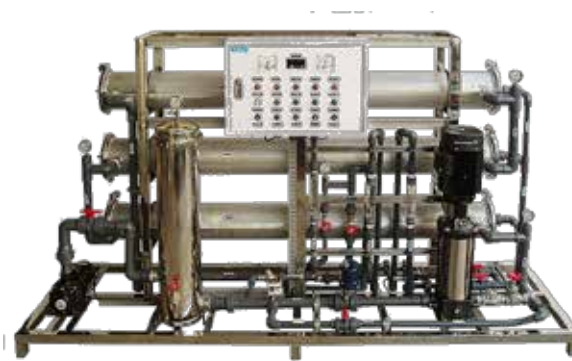


### Current Scenario

- No natural supply of potable water- over dependent on tube well supply
- Yellowish and poor water quality supply

## The Necessity & Societal Benefits

- SWRO DESAL with max. capacity of 0.5 MLD can benefit 3,300 residents (150 Litre/person) for sustainable daily freshwater supply.
- The clean and sustainable water supply is the catalyst to revive the tourism industry





# AMTEC'S Products



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# 1 — TYPE A – UTM Membrane

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**Output: 40,000 litre/day (2 unit for 80,000Litre/day)**

**Water source:** Surface water/ River water

- Treated water production for drinking water with the capacity of 80,000 litre/day.
- To cater for 5,000 users.
- 2 units installed at Kg. Sinarot for CSR earthquake relief.

## **ADVANTAGES:**

- Portable system
- Beneficial to 5,000 users
- High water quality <0.1 NTU
- 99.9 % bacteria and viruses removal
- 100% colloidal removal
- Low cost and maintenance
- No chemicals are required
- Includes back flushing system for cleaning purpose

## **SPECIFICATION:**

- Max Capacity : 80,000 L/day (2 unit)
- Operating pressure : 1-10 bar
- Operating temperature : Max 50 ° C
- pH range : 3.0-12.0
- Conductivity : Raw (>500µS/cm)  
: Filtrate (<100µS/cm)



**PRICING: USD185,000.00 /unit**

## 2 — TYPE B – UTM Membrane

**Output: 20,000 litre/day.**

**Water source:** Surface water/ River water

- Treated water production for drinking water with the capacity of 20,000 litre/day.
- To cater for 2,000 users.
- 1 units installed at Kg. Rumidako, Kiulu for CSR on water shortage.

### **ADVANTAGES:**

- Portable system
- Beneficial to 2,000 users
- High water quality <0.1 NTU
- 99.9 % bacteria and viruses removal
- 100% colloidal removal
- Low cost and maintenance
- No chemicals are required
- Includes back flushing system for cleaning purpose

### **SPECIFICATION:**

- Max Capacity : 20,000 L/day
- Operating pressure : 1-10 bar)
- Operating temperature : Max 50 ° C
- pH range : 3.0-12.0
- Conductivity : Raw (>500µS/cm)  
: Filtrate (<100µS/cm)



**PRICING: USD120,000.00**



### 3 — TYPE C – UTM Membrane

**Output: 1,000 litre/day.**

**Water source:** Surface water/ River water

- **Treated water production for drinking water with the capacity of 2,000 litre/day.**
- **To cater for 500 users.**
- **4 units delivered to Jabatan Air Kelantan as CSR water purification system in disaster.**

**BENEFITS:**

- Integrated mobile RO water purification unit is specialized design using Ultrafiltration and Reverse Osmosis membrane to produced a drinking water.
- The unit can treats any water source including river water, surface water, turbid and contaminated water sources.

**SPECIFICATION:**

- Max Capacity : 1000 L/day
- Operating pressure : 1-7 bar
- Operating temperature : Max 50 ° C
- pH range : 3.0-12.0
- Conductivity : <100µS/cm

**PRICING: USD35,000.00**





## 4 — TYPE D – UTM Membrane

**Output:** 6,000 litre/day (Utilities Water),  
1,000 litre/day (Drinking Water)

**Water source:** Brackish water/ Seawater

- 1 units installed at Endao as CSR unit.

### ADVANTAGES:

- Portable system
- Beneficial to 300-500 users
- High water quality < 0.1 NTU
- 99.9 % bacteria and viruses removal
- 100% colloidal removal
- Low cost and maintenance
- No chemicals are required
- Includes back flushing system for cleaning purpose

### SPECIFICATION:

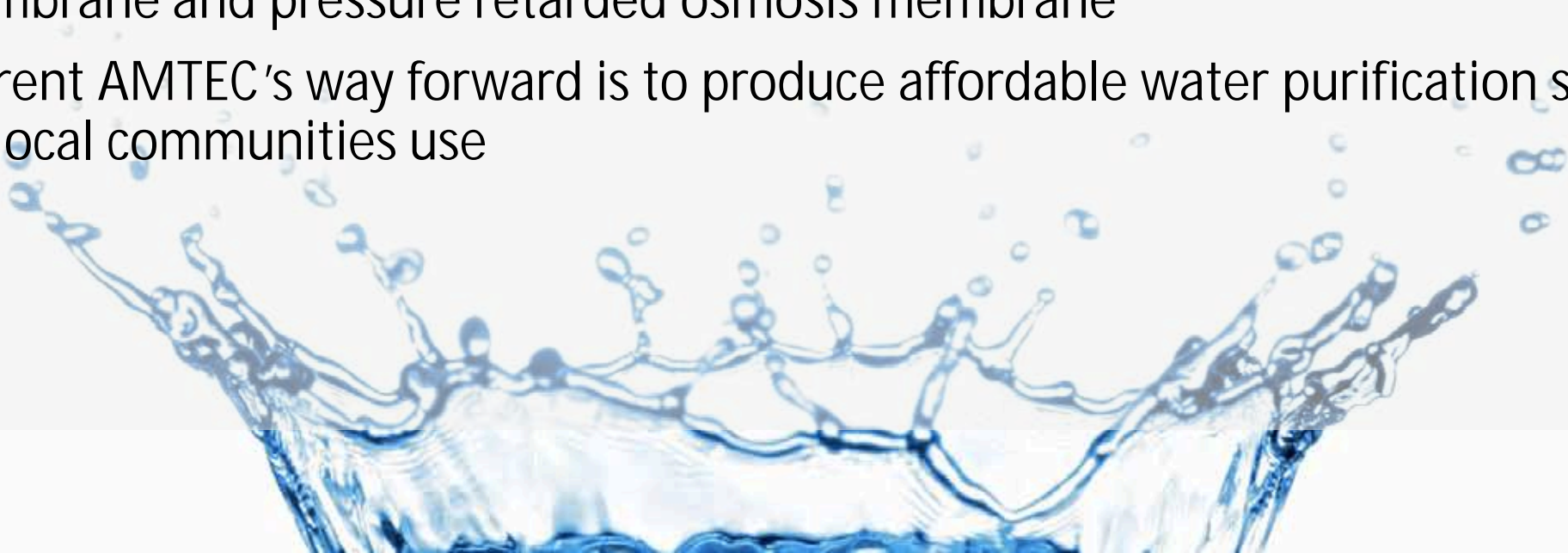
- Max Capacity : 6000 L/day
- Operating pressure : Low (1-5 bar)
- : High (50-70 bar)
- Operating temperature : Max 50 ° C
- pH range : 3.0-12.0
- Conductivity : Raw (>30 mS/cm)
- : 2<sup>nd</sup> pass RO (<400µS/cm)



**PRICING: USD75,000.00**

# Conclusions

- AMTEC is now in the right direction to become a hub of membrane-based technology for nation human capital development and wealth creation for the future, especially in the niche area of water reclamation
- Apart from FO, photocatalytic and adsorptive membranes, AMTEC also gives attention to the development of membrane contactor, graphene based membrane and pressure retarded osmosis membrane
- Current AMTEC's way forward is to produce affordable water purification system for local communities use



# AMTEC'S Video



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# THANK YOU

Juhana Jaafar, PhD  
Associate Professor

[juhana@petroleum.utm.my](mailto:juhana@petroleum.utm.my)

[www.utm.my/amtec](http://www.utm.my/amtec) | [fcee.utm.my/juhana/](http://fcee.utm.my/juhana/)



HAKONE, 2009